

A conservative diffuse-interface method for the simulation of compressible two-phase flows with turbulence and acoustics

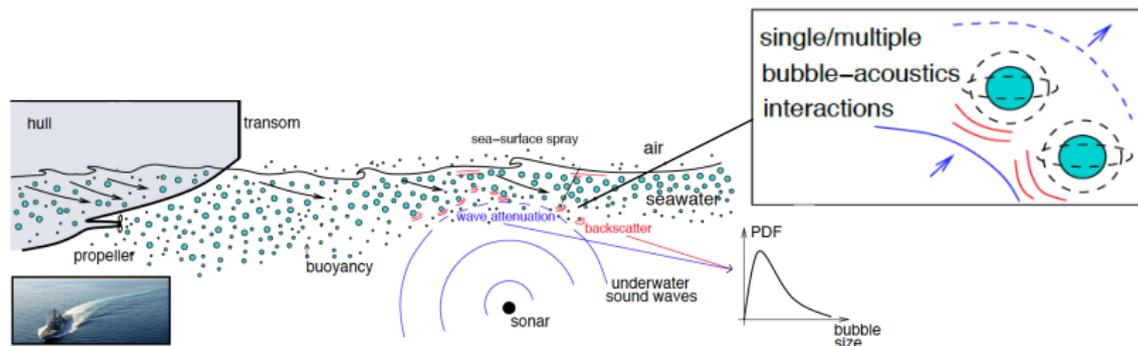
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Introduction and Motivation



(courtesy: Dr. J. Urzay)

applications

- bubble acoustics
- high pressure liquid fuel injection

challenges

- Need to **maintain thermodynamic consistency** at the interface.
- Numerical study of turbulence and acoustics require
 - **a stable method for long-time integrations**
 - **a non-dissipative method**
 - **a conservative method**

Five-equation model

$$\frac{\partial \phi_1}{\partial t} + \vec{u} \cdot \vec{\nabla} \phi_1 = 0,$$

$$\frac{\partial \rho_1 \phi_1}{\partial t} + \vec{\nabla} \cdot (\rho_1 \vec{u} \phi_1) = 0,$$

$$\frac{\partial \rho_2 \phi_2}{\partial t} + \vec{\nabla} \cdot (\rho_2 \vec{u} \phi_2) = 0,$$

$$\frac{\partial \rho \vec{u}}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u} \otimes \vec{u} + p \mathbf{1}) = 0,$$

$$\frac{\partial \rho(e + k)}{\partial t} + \vec{\nabla} \cdot (\rho H \vec{u}) = 0,$$

Closure:

$$p = f(\rho_1 \phi_1, \rho_2 \phi_2, \rho e, \phi_1)$$

[Allaire et al., *JCP*, 2002]

diffuse-interface (DI) vs sharp-interface methods (SI)

sharp-interface methods

- Hermann, *CTR Summer Proc.*, 2016 - geometric volume of fluid (VoF)
- Huber et al., *JCP*, 2015 - level set
- He et al., *JCP*, 2015 - algebraic VoF

advantages of DI methods over SI methods

- less expensive
- easy load balancing and parallel scalability
- conserves mass of each phase discretely

[Mirjalili, *Jain* & Dodd, *CTR Annual Research Briefs*, 2017]

State-of-the-art methods

five-equation model

- Perigaud & Saurel, *JCP*, 2005 → capillary and viscous effects
- Shukla et al., *JCP*, 2010 & Tiwari et al., *JCP*, 2013 → interface regularization
- Chiapolino et al., *JCP*, 2017 → unstructured grids

Other models

- Abgrall, *JCP*, 1996 → four-equation model
- Saurel & Abgrall, *JCP*, 1999 → seven-equation model

Summary

- five-equation model is the most preferred choice
- no previous implementation using non-dissipative schemes
- all interface regularization (sharpening) terms are in non-conservative form
- no previous study of bubble acoustics in turbulent environment

[*Jain*, Mani & Moin, *CTR Annual Research Briefs*, 2018]

Proposed model

$$\begin{aligned} \frac{\partial \phi_1}{\partial t} + \vec{\nabla} \cdot (\vec{u} \phi_1) &= \phi_1 (\vec{\nabla} \cdot \vec{u}) + \vec{\nabla} \cdot \vec{a} \\ \frac{\partial \rho_l \phi_l}{\partial t} + \vec{\nabla} \cdot (\rho_l \vec{u} \phi_l) &= \vec{\nabla} \cdot R_l \quad l = 1, 2 \\ \frac{\partial \rho \vec{u}}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u} \otimes \vec{u} + p \mathbf{1}) &= \vec{\nabla} \cdot \underline{\underline{\tau}} + \vec{\nabla} \cdot (\vec{f} \otimes \vec{u}) \\ \frac{\partial E}{\partial t} + \vec{\nabla} \cdot (\vec{u} E) + \vec{\nabla} \cdot (p \vec{u}) &= \vec{\nabla} \cdot (\vec{f} k) + \vec{\nabla} \cdot (\underline{\underline{\tau}} \cdot \vec{u}) + \sum_{l=1}^2 \vec{\nabla} \cdot (\rho_l h_l \vec{a}_l) \end{aligned}$$

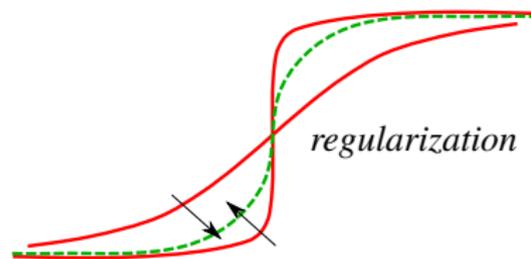
Closure:

$$p = \frac{\rho e + \left(\frac{\phi \beta_1}{\alpha_1} + \frac{(1-\phi) \beta_2}{\alpha_2} \right)}{\left(\frac{\phi}{\alpha_1} + \frac{1-\phi}{\alpha_2} \right)}$$

[**Jain**, Mani & Moin, *CTR Annual Research Briefs*, 2018]

Improvements over the state-of-the-art methods

- ① conservative form of regularization terms.
 - mass of each phase, momentum and energy is discretely conserved.
- ② satisfies interface equilibrium condition.
- ③ central-difference scheme (non-dissipative).
- ④ volume fraction equation \Rightarrow bounded ϕ .
- ⑤ mass balance equation \Rightarrow consistent with ϕ .
- ⑥ momentum equation \Rightarrow kinetic energy conservation.
- ⑦ energy equation \Rightarrow approximate entropy conservation.



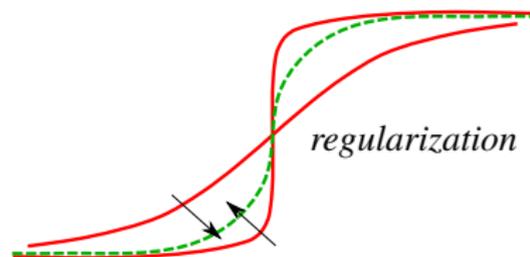
interface equilibrium condition

If $u_i^k = u_0$ and $p_i^k = p_0$ then, $u_i^{k+1} = u_0$ and $p_i^{k+1} = p_0$ should be satisfied.
 (Abgrall, *JCP*, 1996)

[*Jain, Mani & Moin, CTR Annual Research Briefs, 2018*]

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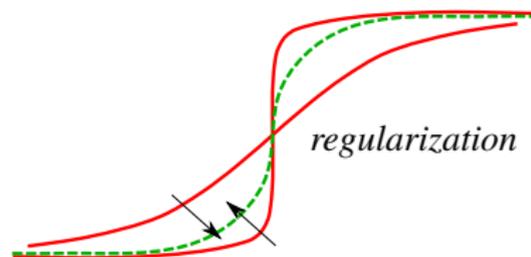
volume fraction advection equation

$$\frac{\partial \phi_1}{\partial t} + \vec{\nabla} \cdot (\vec{u} \phi_1) = \phi_1 (\vec{\nabla} \cdot \vec{u}) + \vec{\nabla} \cdot \vec{a}$$

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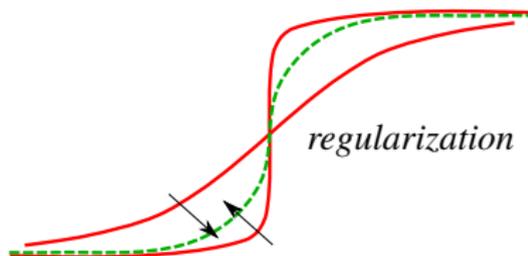
mass balance equation

$$\frac{\partial \rho_l \phi_l}{\partial t} + \vec{\nabla} \cdot (\rho_l \vec{u} \phi_l) = \vec{\nabla} \cdot R_l \quad l = 1, 2$$

[**Jain**, Mani & Moin, *CTR Annual Research Briefs*, 2018]

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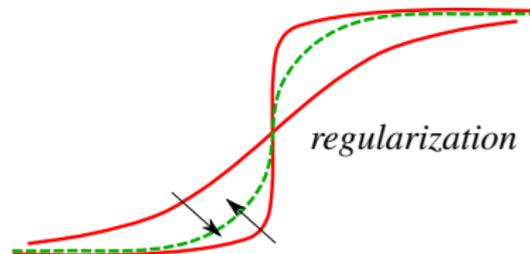
momentum equation

$$\frac{\partial \rho \vec{u}}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u} \otimes \vec{u} + p \mathbf{1}) = \vec{\nabla} \cdot \underline{\underline{\tau}} + \vec{\nabla} \cdot (\vec{f} \otimes \vec{u})$$

[*Jain, Mani & Moin, CTR Annual Research Briefs, 2018*]

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energy equation

$$\frac{\partial E}{\partial t} + \vec{\nabla} \cdot (\vec{u}E) + \vec{\nabla} \cdot (p\vec{u}) = \vec{\nabla} \cdot (\vec{f}k) + \vec{\nabla} \cdot (\underline{\underline{\tau}} \cdot \vec{u}) + \sum_{l=1}^2 \vec{\nabla} \cdot (\rho_l h_l \vec{a}_l)$$

[Jain, Mani & Moin, *CTR Annual Research Briefs*, 2018]

Verification cases

Fluid properties:

Stiffened gas equation of state: $p = (\gamma - 1)\rho e - \pi$

	air	water	kerosene
ρ (kg/m ³)	1.225	997	820
μ (N/m ²)	0.0000181	0.00089	0.00164
γ	1.4	4.4	4.4
π (MPa)	0	600	326.6
c (m/s)	338.1	1627.4	1324

Analytical solution:

Rayleigh-Plesset equation in 2D bounded domain

$$\frac{P_B(t) - P_S(t)}{\rho_L} = \ln\left(\frac{S}{R}\right) \left\{ R\ddot{R} + (\dot{R})^2 \right\} + \left(\frac{R^2 - S^2}{2S^2} \right) + \frac{2\nu_L \dot{R}}{R} + \frac{\sigma}{\rho_L R}$$

Pressure driven bubble oscillation

Physical parameters:

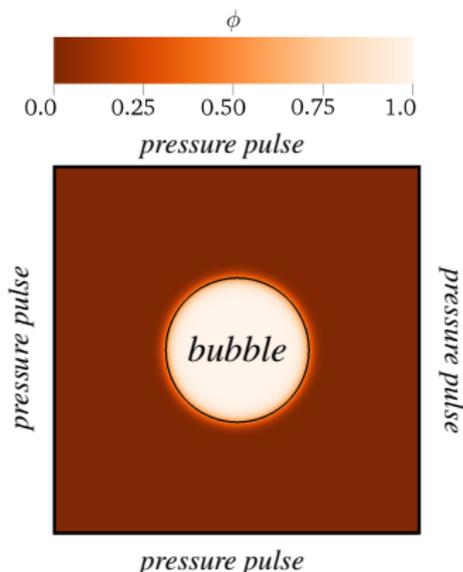
- Fluids: *air, water*
- Domain: $10\mu\text{m} \times 10\mu\text{m}$
- Bubble diameter: $4\mu\text{m}$

Simulation parameters:

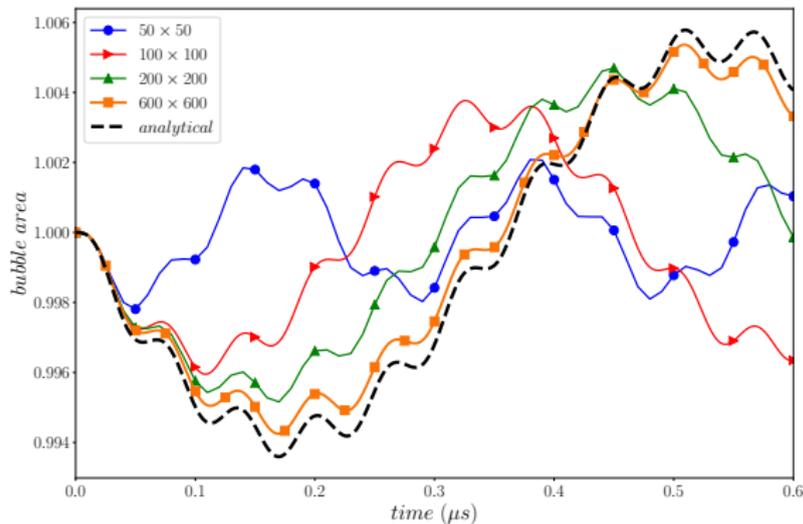
- Grid: 50×50 , 100×100 , 200×200 and 600×600
- Total time: $50\mu\text{s}$
- Interface: $\Gamma = 1$, $\epsilon = \Delta x$

Pressure pulse boundary condition:

- Pressure: *Dirichlet*:
 $10^5 \{1 + 0.1 \sin(10\omega_c t)\}$
- Velocity: *Neumann*

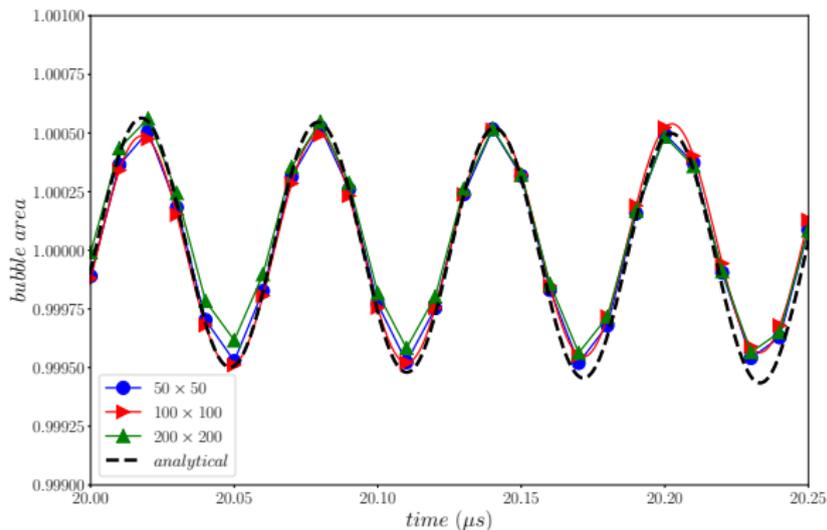


Initial transient bubble response



Solution converges to the analytical solution

Bubble response at later times



Long time solution is very accurate even on a coarse grid!

Plane acoustic wave incident on an air-water interface

Physical parameters:

- Fluids: *air, water*
- Domain: $10\mu\text{m} \times 0.1\mu\text{m} \times 0.1\mu\text{m}$
- Interface location: $5\mu\text{m}$

Simulation parameters:

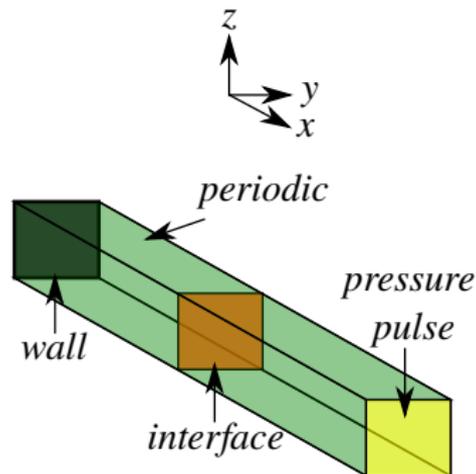
- Grid: $1000 \times 10 \times 10$
- Time step: $\Delta t = 1\text{ps}$
- Total time: $1\mu\text{s}$
- Interface: $\Gamma = 1, \epsilon = \Delta x$

Pressure pulse boundary condition:

$t < 614.5\text{ps}$:

- Pressure: *Dirichlet*:
 $10^5 \{1 - 0.5 \sin(c \frac{2\pi}{\lambda} t)\}$
- Velocity: *Neumann*

$t > 614.5\text{ps}$: *wall BC*



Reflection and transmission at the flat interface

$$\mathbb{R} = \frac{Z_a - Z_w}{Z_a + Z_w} = -0.999516$$

$$\mathbb{T} = \frac{2Z_a}{Z_a + Z_w} = 4.8 \times 10^{-3}$$

Oblique acoustic wave incident on an water-kerosene interface

Snell's law:

$$\frac{\sin(\theta_i)}{c_1} = \frac{\sin(\theta_t)}{c_2}$$

$$\theta_i = \theta_r$$

Total internal reflection:

$$\sin(\theta_t) = \left(\frac{c_2}{c_1}\right)\sin(\theta_i)$$

For,

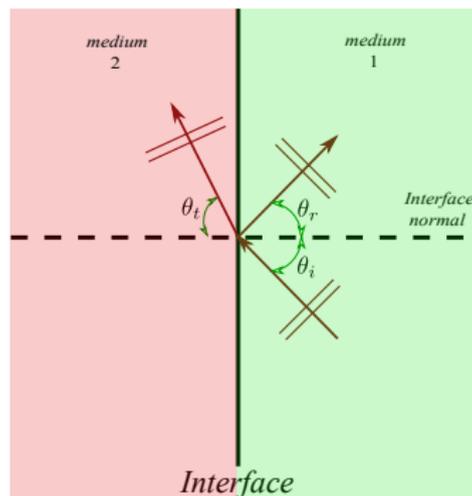
$$c_2 > c_1 \Rightarrow \theta_t > \theta_i.$$

$$\therefore \exists \theta_c \mid \forall \theta_i > \theta_c \nexists \theta_t$$

\Rightarrow Total internal reflection

Critical angle:

$$\sin(\theta_c) = \frac{c_1}{c_2}$$



Continued

Physical parameters:

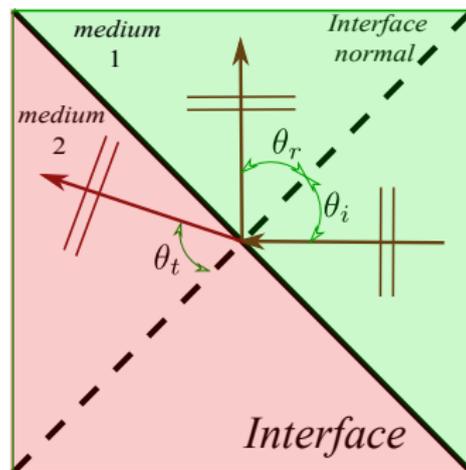
- Fluids: *water, kerosene*
- Domain: $10\mu\text{m} \times 10\mu\text{m}$

Simulation parameters:

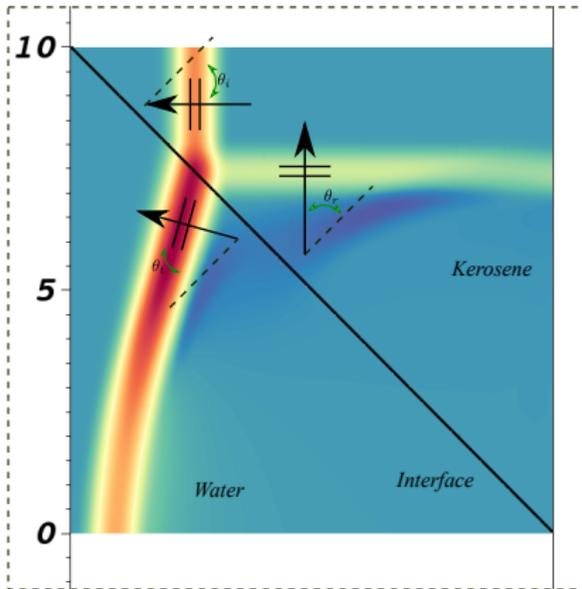
- Grid: 1000×1000
- Interface: $\Gamma = 1, \epsilon = \Delta x$

Case:

$$\begin{aligned}\theta_i &= 45^0 \\ \theta_r &= 45^0 \\ \theta_t &= 60.358^0 \\ \theta_c &= 54.5^0\end{aligned}$$



Reflection and transmission at the interface



Conclusion

summary

- A conservative diffuse-interface method for simulation of compressible two-phase flows with acoustics.
- Improvements to the state-of-the-art methods:
 - discrete mass, momentum and energy conservation
 - central-difference scheme (non-dissipative)
 - stable method for long-time integrations
 - thermodynamic consistency at the interface
 - kinetic energy and entropy conservation

ongoing and future work

- compressible Rayleigh-Taylor simulation
- extension to acoustics in turbulent environments
- detection of bubble size distribution using acoustic signals

THANK YOU

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Franklin P. and Caroline M. Johnson Fellowship

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PSAAP-II Center at Stanford (DoE Grant #107908)



References:

Jain, S, S; Mani, A & Moin, P, 'A conservative diffuse-interface method for the simulation of compressible two-phase flows with turbulence and acoustics', *Center for Turbulence Research, Annual Research Briefs (December 2018)*.

Model derivation

volume fraction advection equation

$$\frac{\partial \phi}{\partial t} + \vec{\nabla} \cdot (\vec{u}\phi) = \phi(\vec{\nabla} \cdot \vec{u}) + \vec{\nabla} \cdot \left[\Gamma \left\{ \epsilon \vec{\nabla} \phi - \phi(1 - \phi)\vec{n} \right\} \right],$$

boundedness theorem

If $0 \leq \phi_i^k \leq 1$ is satisfied for $k = 0$, then $0 \leq \phi_i^k \leq 1$ holds $\forall k > 0$ provided

$$\frac{\epsilon}{\Delta x} \geq \frac{(|u|_{max} + 1)}{2},$$

and

$$\Delta t \leq \frac{1}{\left(\frac{2\Gamma\epsilon}{\Delta x^2} \right) - \left(\frac{u_{i+1}^k - u_{i-1}^k}{2\Delta x} \right)},$$

are satisfied on a uniform one-dimensional grid, where k is the time step index and i is the grid index.

(motivated from Mirjalili et al., *JCP*, 2018)

[*Jain*, Mani & Moin, *CTR Annual Research Briefs*, 2018]

Continued

mass balance equation

$$\frac{\partial \rho_1 \phi}{\partial t} + \vec{\nabla} \cdot (\rho_1 \vec{u} \phi) = \vec{\nabla} \cdot \left[\rho_{01} \Gamma \left\{ \epsilon \vec{\nabla} \phi - \phi (1 - \phi) \vec{n} \right\} \right]$$

In the incompressible limit, it reduces to the volume fraction advection equation.

- Modified momentum equation \Rightarrow conservative kinetic energy.
- Modified energy equation \Rightarrow approximate conservation of entropy.

entropy conservation lemma

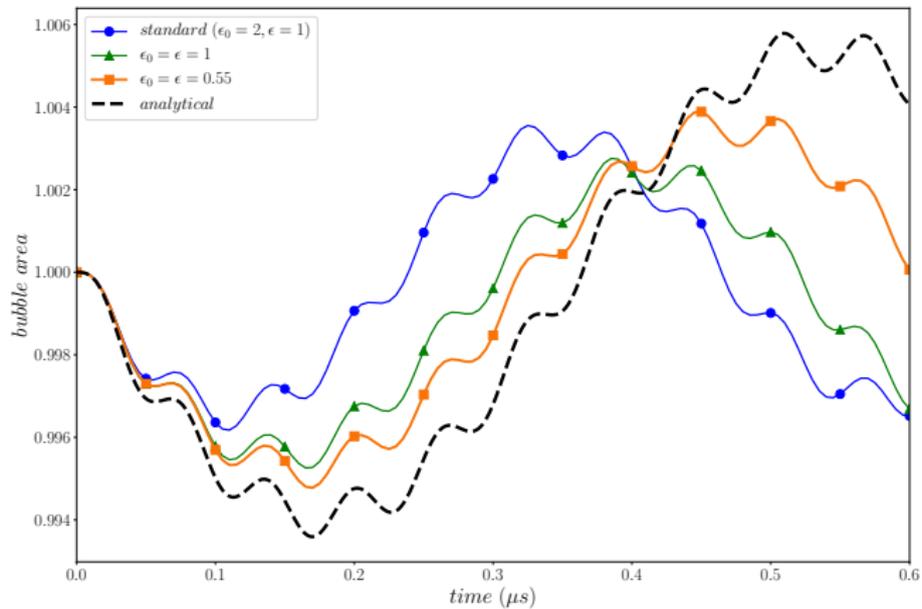
Let s_l be the physical entropy and T_l be the temperature of phase l , then the form of internal energy equation that satisfies

$$\sum_{l=1}^2 \left[\rho_l \phi_l T_l \frac{Ds_l}{Dt} \right] = 0 \quad (1)$$

in the inviscid limit is

$$\frac{\partial \rho e}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u} e) + \vec{\nabla} \cdot (p \vec{u}) - \vec{u} \cdot \vec{\nabla} p = \sum_{l=1}^2 \{ h_l \vec{\nabla} \cdot (\rho_l \vec{a}_l) \} \quad (2)$$

[**Jain**, Mani & Moin, *CTR Annual Research Briefs*, 2018]

Effect of ϵ 

Plane acoustic wave in water

Physical parameters:

- Fluid: *water*
- Domain: $10\mu\text{m} \times 0.1\mu\text{m} \times 0.1\mu\text{m}$

Simulation parameters:

- Grid: $1000 \times 10 \times 10$
- Time step: $\Delta t = 1\text{ps}$
- Total time: $1\mu\text{s}$
- Interface: $\Gamma = 1$, $\epsilon = \Delta x$

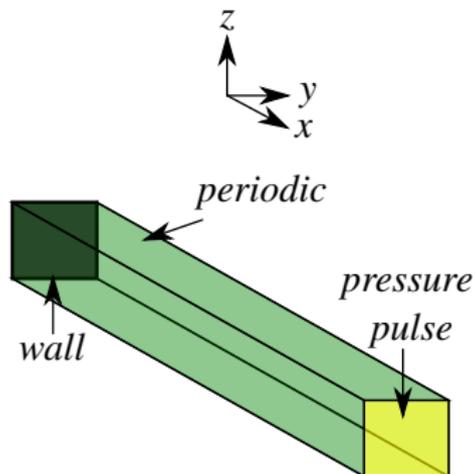
Pressure pulse boundary condition:

$t < 614.5\text{ps}$:

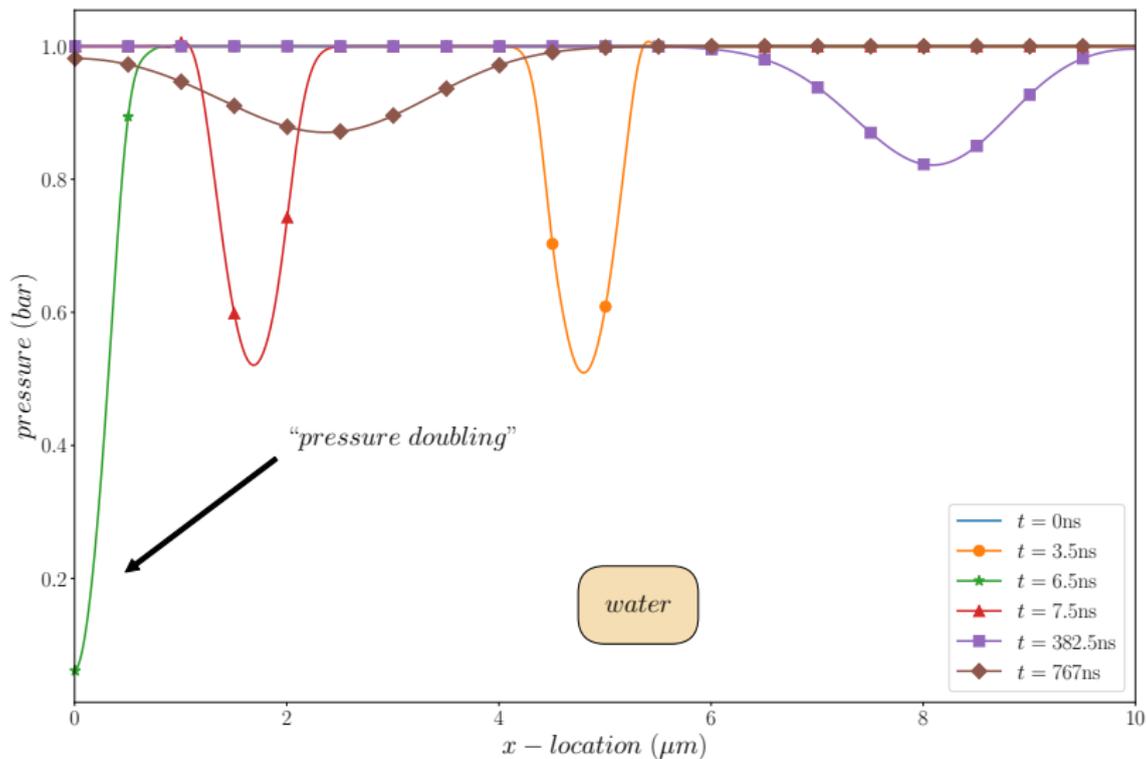
- Pressure: Dirichlet:
 $10^5(1 - 0.5\sin(5112583866t))$
- Velocity: Neumann

$t > 614.5\text{ps}$:

- Wall BC.



Continued



Plane acoustic wave incident on an air-water interface

