

# Lecture 14 - Model Predictive Control

## Part 1: The Concept

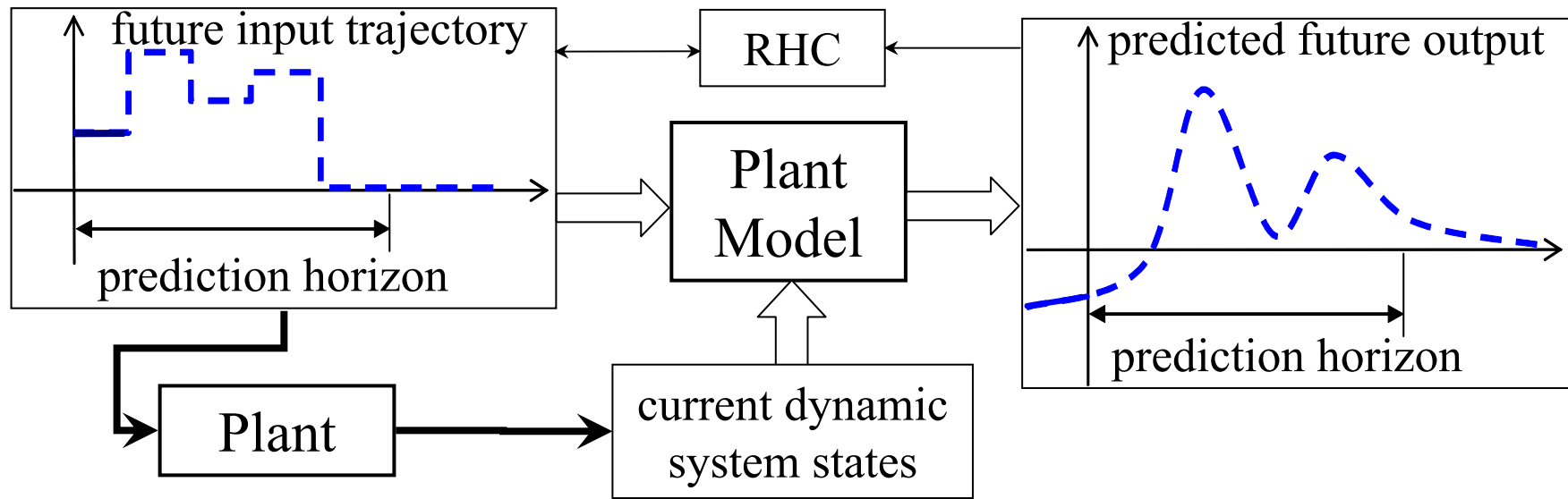
- History and industrial application resource:
  - Joe Qin, survey of industrial MPC algorithms
  - <http://www.che.utexas.edu/~qin/cpcv/cpcv14.html>
- Emerging applications
- State-based MPC
  - Conceptual idea of MPC
  - Optimal control synthesis
- Example
  - Lateral control of a car
- Stability
- Lecture 15: Industrial MPC

# MPC concept

- MPC = Model Predictive Control
- Also known as
  - DMC = Dynamical Matrix Control
  - GPC = Generalized Predictive Control
  - RHC = Receding Horizon Control
- Control algorithms based on
  - Numerically solving an optimization problem at each step
  - Constrained optimization – typically QP or LP
  - Receding horizon control
- More details need to be worked out for implementation

# Receding Horizon Control

- Receding Horizon Control concept



- At each time step, compute control by solving an open-loop optimization problem for the prediction horizon
- Apply the first value of the computed control sequence
- At the next time step, get the system state and re-compute

# Current MPC Use

- Used in a majority of existing multivariable control applications
- Technology of choice for many new advanced multivariable control application
- Success rides on the computing power increase
- Has many important practical advantages

# MPC Advantages

- Straightforward formulation, based on well understood concepts
- Explicitly handles constraints
- Explicit use of a model
- Well understood tuning parameters
  - Prediction horizon
  - Optimization problem setup
- Development time much shorter than for competing advanced control methods
- Easier to maintain: changing model or specs does not require complete redesign, sometimes can be done on the fly

# History

- First practical application:
  - DMC – Dynamic Matrix Control, early 1970s at Shell Oil
  - Cutler later started Dynamic Matrix Control Corp.
- Many successful industrial applications
- Theory (stability proofs etc) lagging behind 10-20 years.
- See an excellent resource on industrial MPC
  - Joe Qin, Survey of industrial MPC algorithms
  - history and formulations
  - <http://www.che.utexas.edu/~qin/cpcv/cpcv14.html>

# Some Major Applications

Area	DMC Corp.	Setpoint Inc.	Honeywell Profimatics	Adersa	Treiber Controls	Total
Refining	360	320	290	280	250	1500
Petrochemicals	210	40	40	-	-	290
Chemicals	10	20	10	3	150	193
Pulp and Paper	10	-	30	-	5	45
Gas	-	-	5	-	-	5
Utility	-	-	2	-	-	2
Air Separation	-	-	-	-	5	5
Mining/Metallurgy	-	2	-	7	6	15
Food Processing	-	-	-	41	-	41
Furnaces	-	-	-	42	-	42
Aerospace/Defense	-	-	-	13	-	13
Automotive	-	-	-	7	-	7
Other	10	20	-	45	-	75
<b>Total</b>	<b>600</b>	<b>402</b>	<b>377</b>	<b>438</b>	<b>416</b>	<b>2233</b>
First App	DMC:1985	IDCOM-M:1987 SMCA:1993	PCT:1984 RMPCT:1991	IDCOM:1973 HIECON:1986	OPC:1987	
Largest App	603x283	35x28	28x20	-	24x19	

- From Joe Qin, <http://www.che.utexas.edu/~qin/cpcv/cpcv14.html>
- 1995 data, probably 1-2 order of magnitude growth by now

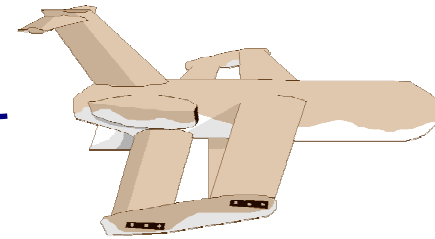
# Emerging MPC applications

- Nonlinear MPC
  - just need a computable model (simulation)
  - NLP optimization
- Hybrid MPC
  - discrete and parametric variables
  - combination of dynamics and discrete mode change
  - mixed-integer optimization (MILP, MIQP)
- Engine control
- Large scale operation control problems
  - Operations management (control of supply chain)
  - Campaign control



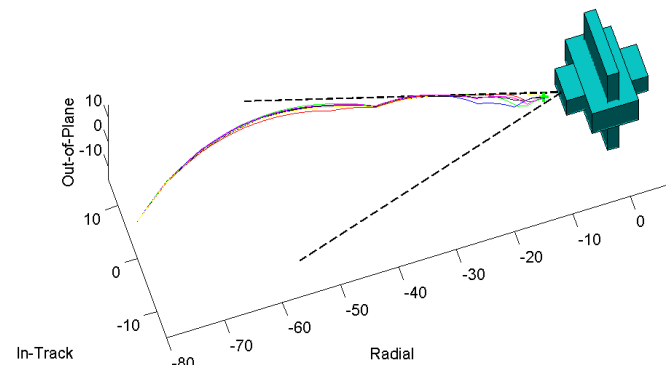
# Emerging MPC applications

- Vehicle path planning and control
  - nonlinear vehicle models
  - world models
  - receding horizon preview



# Emerging MPC applications

- Spacecraft rendezvous with space station
  - visibility cone constraint
  - fuel optimality
- Underwater vehicle guidance
- Missile guidance



From Richards & How, MIT

# State-based control synthesis

- Consider single input system for better clarity

$$x(t+1) = Ax(t) + Bu(t)$$

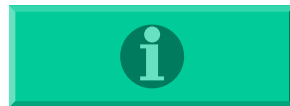
$$y(t) = Cx(t)$$

- Infinite horizon optimal control

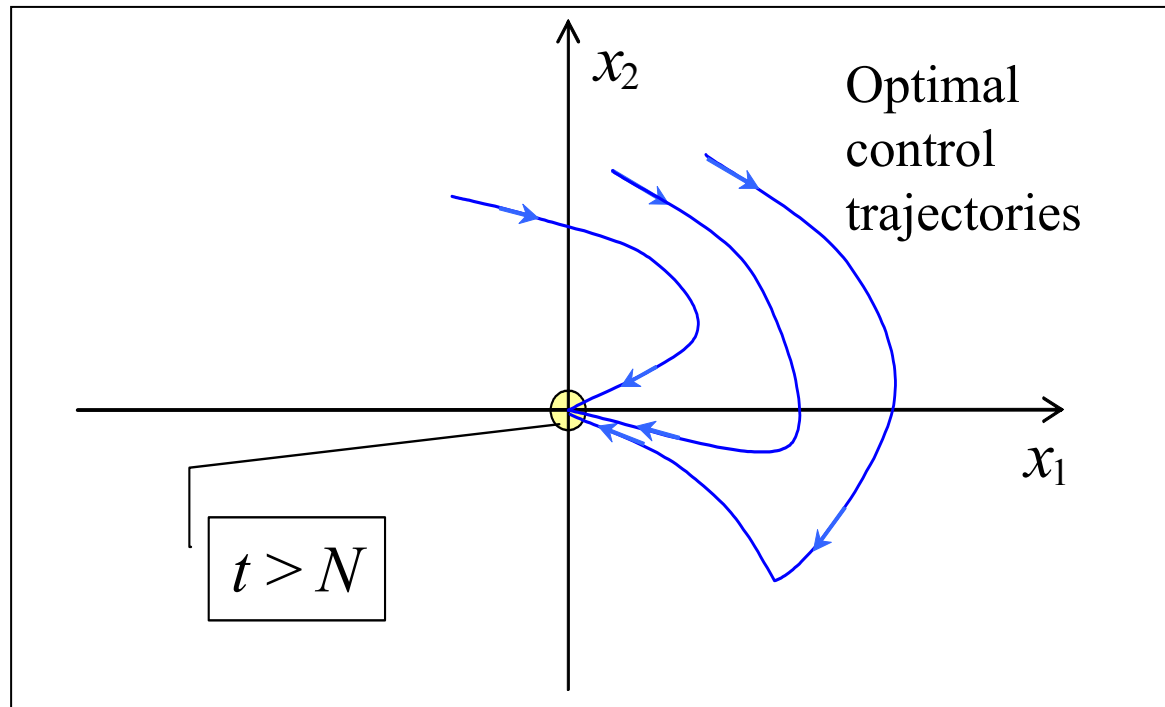
$$\sum_{\tau=t+1}^{\infty} (y(\tau))^2 + r(u(\tau) - u(\tau - 1))^2 \rightarrow \min$$

$$\text{subject to : } |u(\tau)| \leq u_0$$

- Solution = Optimal Control Synthesis



# State-based MPC – concept



- Optimal control trajectories converge to  $(0,0)$
- If  $N$  is large, the part of the problem for  $t > N$  can be neglected
- Infinite-horizon optimal control  $\approx$  horizon- $N$  optimal control

# State-based MPC

- Receding horizon control;  $N$ -step optimal

$$J = \sum_{\tau=t+1}^{t+N} (y(\tau))^2 + r(u(\tau) - u(\tau - 1))^2 \rightarrow \min$$

$$\text{subject to : } |u(\tau)| \leq u_0,$$

$$x(t+1) = Ax(t) + Bu(t)$$

$$y(t) = Cx(t)$$

- Solution  $\approx$  Optimal Control Synthesis

$$x(t) \rightarrow [\text{MPC Problem Solver}] \rightarrow u(t)$$

# Predictive Model

- Predictive system model

$$Y = Gx + HU + Fu \quad \text{initial condition response} + \text{control response}$$

Predicted output

$$Y = \begin{bmatrix} y(t+1) \\ \vdots \\ y(t+N) \end{bmatrix}$$

Future control input

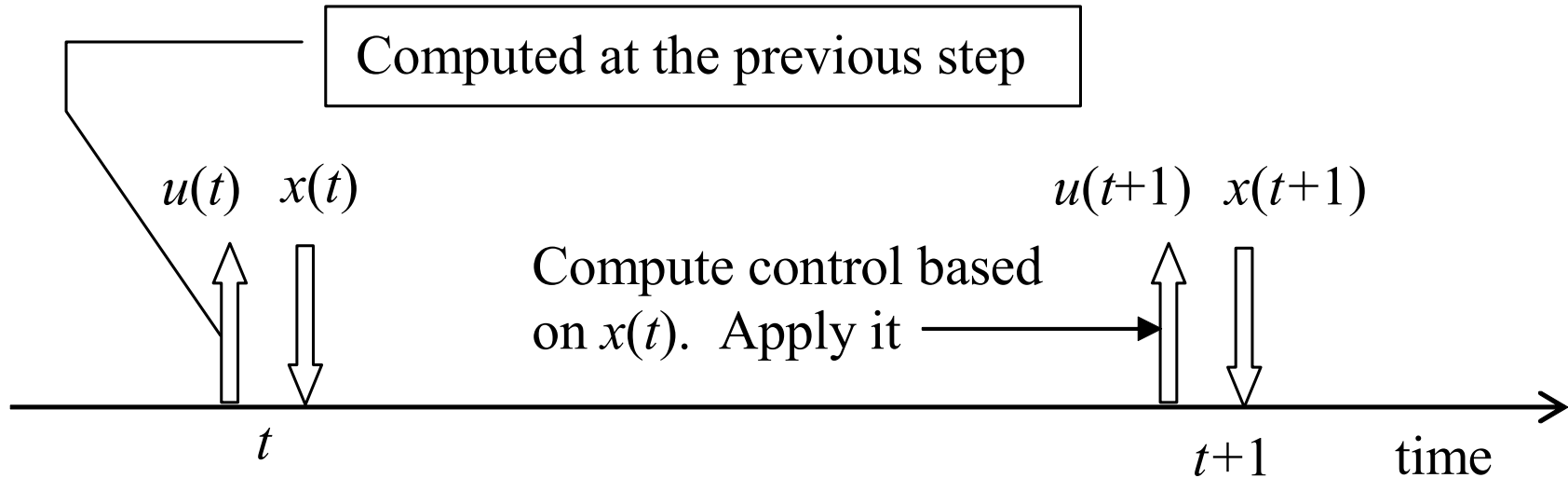
$$U = \begin{bmatrix} u(t+1) \\ \vdots \\ u(t+N) \end{bmatrix}$$

Current state  
(initial condition)  
 $x = x(t)$   
 $u = u(t) \rightarrow$  computed at  
the previous step

- Model matrices

$$G = \begin{bmatrix} CA \\ \vdots \\ CA^n \end{bmatrix} \quad H = \begin{bmatrix} 0 & 0 & \dots & 0 \\ CB & 0 & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ CA^{N-2}B & CA^{N-3}B & \dots & 0 \end{bmatrix} = \begin{bmatrix} h(1) & 0 & \dots & 0 \\ h(2) & h(1) & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ h(N) & h(N-1) & \dots & h(1) \end{bmatrix} \quad F = \begin{bmatrix} h(2) \\ h(3) \\ \vdots \\ h(N+1) \end{bmatrix}$$

# Computations Timeline



- Assume that control  $u$  is applied and the state  $x$  is sampled at the same instant  $t$
- Entire sampling interval is available for computing  $u$

# MPC Optimization Problem Setup

- MPC optimization problem

$$J = Y^T Y + rU^T D^T D U \rightarrow \min$$

$$\text{subject to : } |U| \leq u_0,$$

$$Y = Gx + HU + Fu$$

1<sup>st</sup> difference matrix

$$D = \begin{bmatrix} 1 & -1 & \dots & 0 \\ 0 & 1 & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ 0 & 0 & \dots & 0 \end{bmatrix}$$

- This is a QP problem

- Solution

$$x(t) \rightarrow [\text{MPC Problem, QP Solver}] \rightarrow U \rightarrow u(t+1) = U(1)$$



# QP solution

- QP Problem:

$$AU \leq b$$

$$J = \frac{1}{2}U^T QU + f^T U \rightarrow \min$$

$U = U(t)$  Predicted  
control  
sequence

$$Q = rD^T D + H^T H$$

$$f = H^T (Gx + Fu)$$

$$A = \begin{bmatrix} I \\ -I \end{bmatrix}$$

$$b = \begin{bmatrix} 1 \\ \vdots \\ 1 \end{bmatrix} \cdot u_0$$

- Standard QP codes can be used

# Linear MPC

- Nonlinearity is caused by the constraints
- If constraints are inactive, the QP problem solution is

$$U = Q^{-1} f \quad u = l^T U$$

$$l = \begin{bmatrix} 1 \\ 0 \\ \vdots \\ 0 \end{bmatrix}$$

- This is linear state feedback

$$u(t+1) = l^T (rD^T D + H^T H)^{-1} H^T (Gx(t) + Fu(t))$$

$$u = z^{-1} Kx + z^{-1} Su$$

$$K = l^T (rD^T D + H^T H)^{-1} H^T G$$

$$S = l^T (rD^T D + H^T H)^{-1} H^T F$$

- Can be analyzed as a linear system, e.g., check eigenvalues

$$u = \frac{z^{-1}}{1 - Sz^{-1}} Kx$$

$$zx = Ax + Bu$$

# Nonlinear MPC Stability

- **Theorem** - from Bemporad et al (1994)

Consider a MPC algorithm for a linear plant with constraints. Assume that there is a terminal constraint

$$x(t + N) = 0 \quad \text{for predicted state } x \text{ and}$$

$$u(t + N) = 0 \quad \text{for computed future control } u$$

If the optimization problem is feasible at time  $t$ ,  
then the coordinate origin is stable.

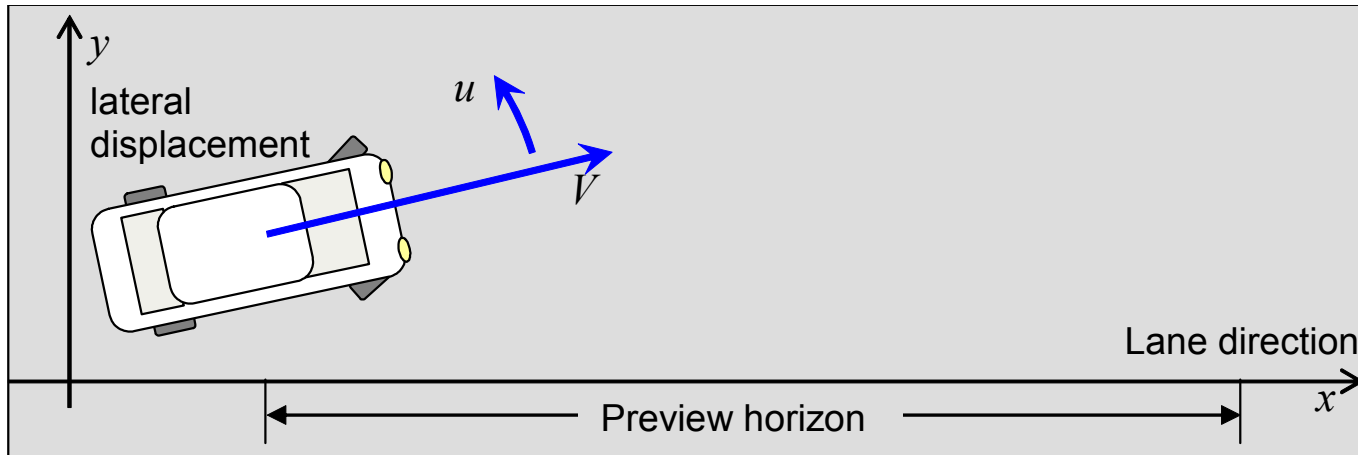
**Proof.**

Use the performance index  $J$  as a Lyapunov function. It decreases along the finite feasible trajectory computed at time  $t$ . This trajectory is suboptimal for the MPC algorithm, hence  $J$  decreases even faster.

# MPC Stability

- The analysis could be useful in practice
  - Theory says a terminal constraint is good
- MPC stability formulations  
(Mayne et al, *Automatica*, 2000)
- Terminal equality constraint
- Terminal cost function
  - Dual mode control – infinite horizon
- Terminal constraint set
  - Increase feasibility region
- Terminal cost and constraint set

# Example: Lateral Control of a Car



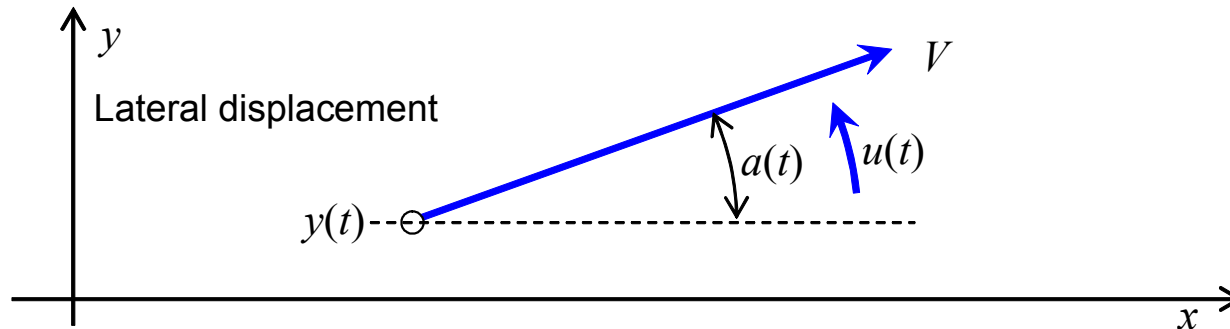
- Preview Control – MacAdam’s driver model (1980)
- Consider predictive control design
- Simple kinematical model of a car driving at speed  $V$

$$\dot{x} = V \cos a$$

$$\dot{y} = V \sin a \quad \text{lateral displacement}$$

$$\dot{a} = u \quad \text{steering}$$

# Lateral Control of a Car - Model



- Assume a straight lane – tracking a straight line
- Linearized system: assume  $a \ll 1$

$$\sin a \approx a \qquad \dot{y} = Va$$

$$\cos a \approx 1 \qquad \dot{a} = u$$

- Sampled-time equations (sampling time  $T_s$ )

$$a(t+1) = a(t) + u(t)T_s$$

$$y(t+1) = y(t) + a(t)VT_s + u(t) \cdot 0.5VT_s^2$$

# Lateral Control of a Car - MPC

State-space system:  $x(t+1) = Ax(t) + Bu(t)$

$$x(t) = \begin{bmatrix} a(t) \\ y(t) \end{bmatrix} \quad A = \begin{bmatrix} 1 & 0 \\ VT_s & 1 \end{bmatrix}, \quad B = \begin{bmatrix} T_s \\ 0.5VT_s^2 \end{bmatrix}$$

Observation:  $y(t) = Cx(t)$   $C = \begin{bmatrix} 0 & 1 \end{bmatrix}$

- Formulate predictive model

$$Y = Gx + HU + Fu$$

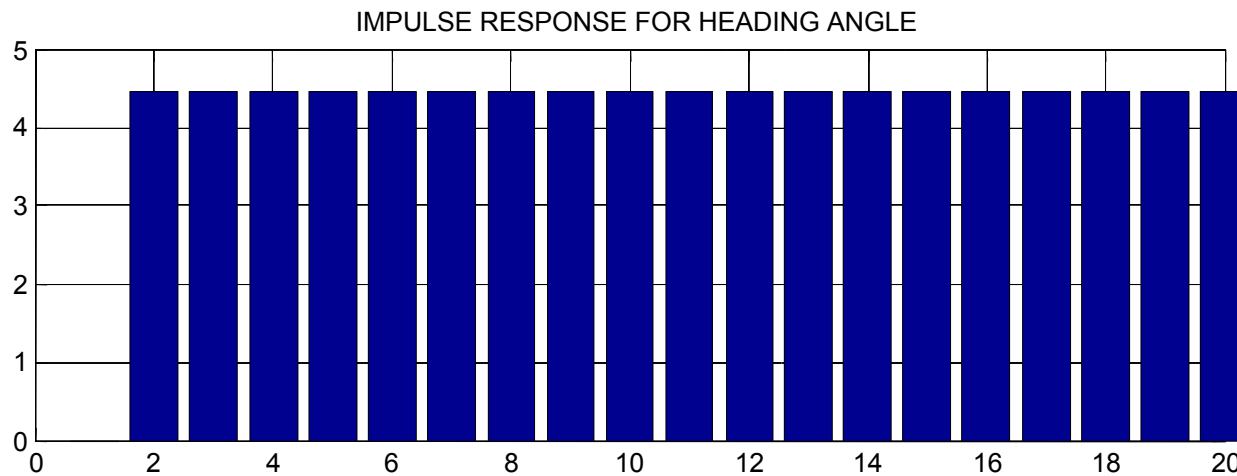
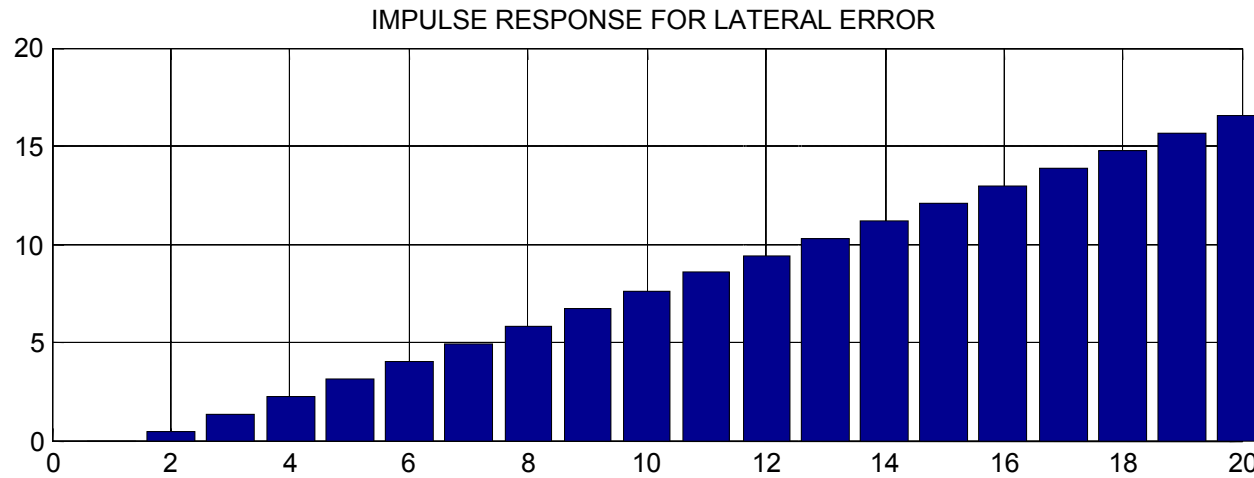
- MPC optimization problem

$$J = (Gx + HU + Fu)^T (Gx + HU + Fu) + rU^T D^T DU \rightarrow \min$$

subject to :  $|U| \leq u_0$ ,

- Solution:  $x(t) \rightarrow [\text{MPC QP}] \rightarrow U \rightarrow u(t+1) = U(1)$

# Impulse Responses

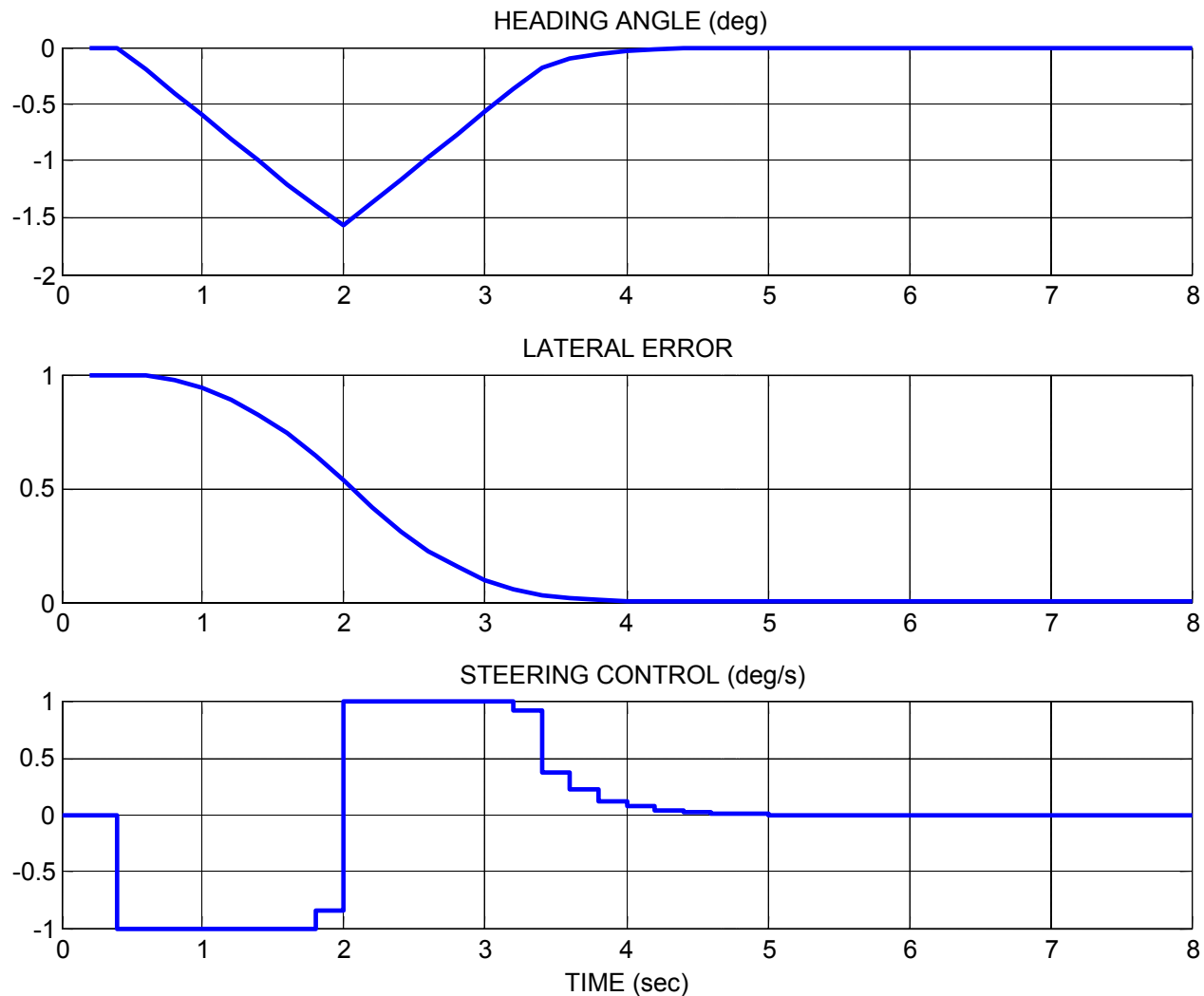




# Lateral Control of a Car - Simulation

## Simulation Results:

- $V = 50$  mph
- Sample time of 200ms
- $N = 20$
- All variables in SI units
- $r = 1$



# Control Design Issues

- Several important issues remain
  - They are not visible in this simulation
  - Will be discussed in Lecture 15 (MPC, Part 2)
- All states might not be available
- Steady state error
  - Need integrator feedback
- Large angle deviation
  - linearized model deficiency
  - introduce soft constraint