

# Solution methods for the Unsteady Incompressible Navier-Stokes Equations



## Unsteady flows

The algorithms we introduced so far are time-marching:

From an initial condition they iterate until a steady-state is reached

The “time”-evolution of the solution is NOT accurate

### Typical Implicit Time-Accurate Scheme

$$\frac{\partial \phi}{\partial t} = F(\phi)$$

Unsteady transport equation

$$\frac{\phi^{m+1} - \phi^m}{\Delta t} = F(\phi^{m+1})$$

1<sup>st</sup> order time integration

$$\frac{3\phi^{m+1} - 4\phi^m + \phi^{m-1}}{2\Delta t} = F(\phi^{m+1})$$

2<sup>nd</sup> order time integration



## Unsteady flows – Implicit Pressure-based

Generic Transport Equation

$$\int_V \frac{\partial \rho \phi}{\partial t} dV + \oint \rho \phi \vec{v} \cdot d\vec{A} = \oint \Gamma_\phi \nabla \phi \cdot d\vec{A} + \int_V S_\phi dV$$

Fully Implicit Discretization

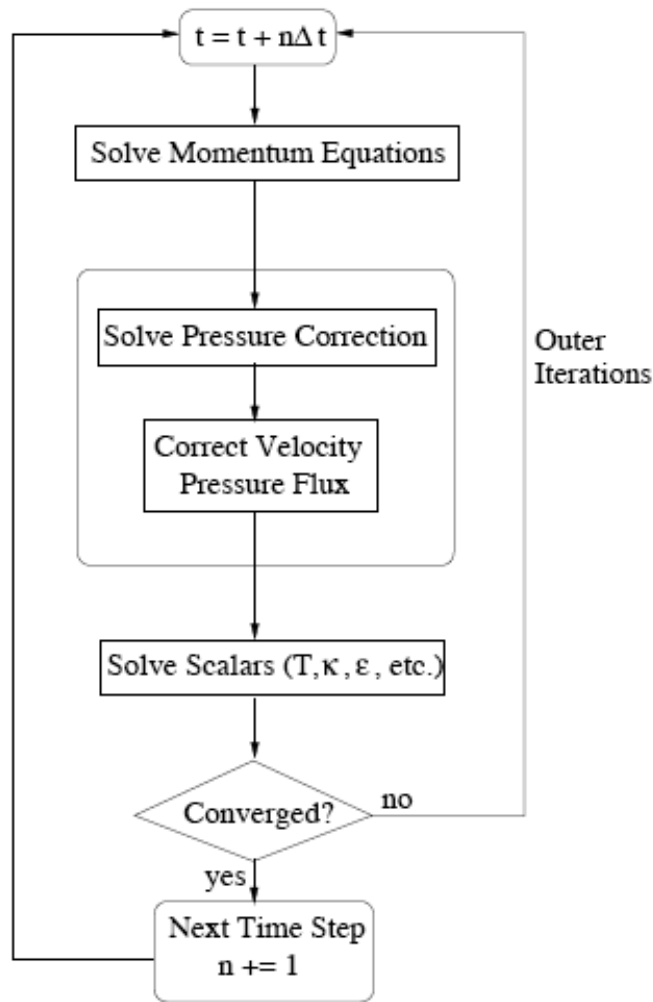
$$\int_V \frac{\partial \rho \phi}{\partial t} dV + \oint \rho^{n+1} \phi^{n+1} \vec{v}^{n+1} \cdot d\vec{A} = \oint \Gamma_\phi^{n+1} \nabla \phi^{n+1} \cdot d\vec{A} + \int_V S_\phi^{n+1} dV$$

Frozen Flux Formulation

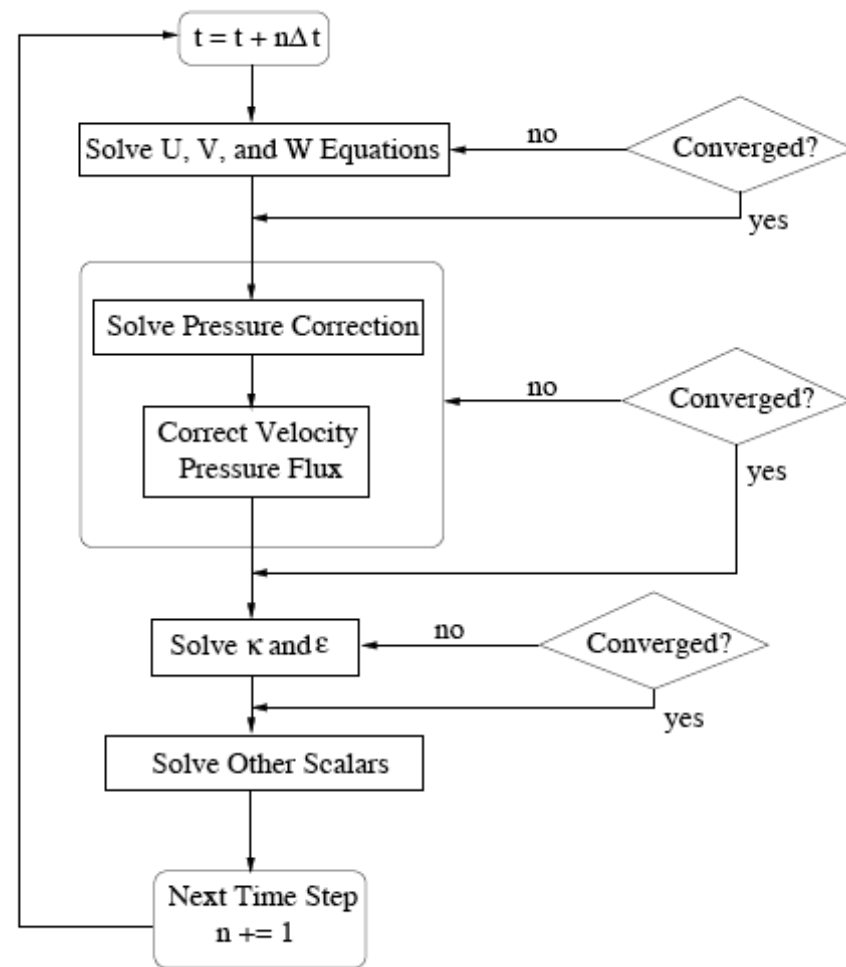
$$\oint \rho \phi \vec{v} \cdot d\vec{A} = \oint \rho^n \phi^{n+1} \vec{v}^n \cdot d\vec{A}$$



# Unsteady flows – Pressure-based Methods



Iterative

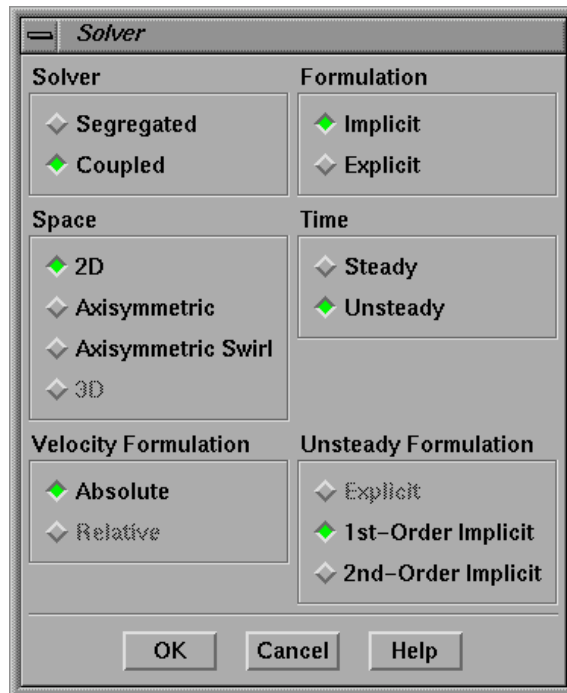


Non-Iterative

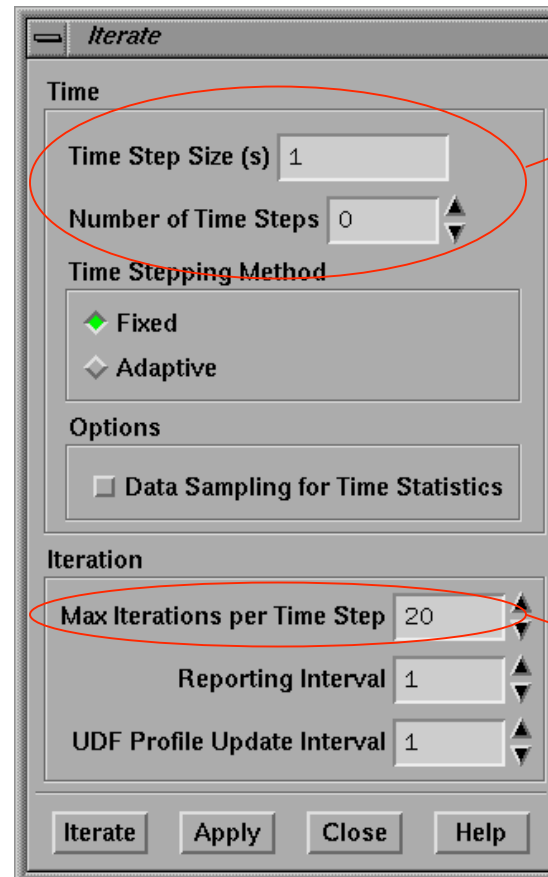


# Unsteady flows – Set Up

Define → Models → Solver



Solve → Iterate



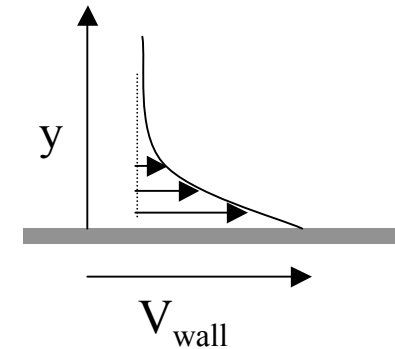
Outer iteration

Inner iteration



## Unsteady Flow – Impulsive start-up of a plate

Again an analytical solution of the Navier-Stokes equations can be derived:



$$u(y = 0, t) = V_{wall}; u(y = \infty, t) = 0$$

Solution in the form  $u = u(y, t)$

The only force acting is the viscous drag on the wall

Navier-Stokes equations

$$\frac{\partial u}{\partial t} = \nu \frac{\partial^2 u}{\partial y^2}$$

Velocity distribution

$$\frac{u(y, t)}{V_{wall}} = 1 - \frac{2}{\sqrt{\pi}} \int_0^{y/2\sqrt{\nu t}} e^{-\chi^2} d\chi = 1 - \text{erf}\left(\frac{y}{2\sqrt{\nu t}}\right)$$

Wall shear stress

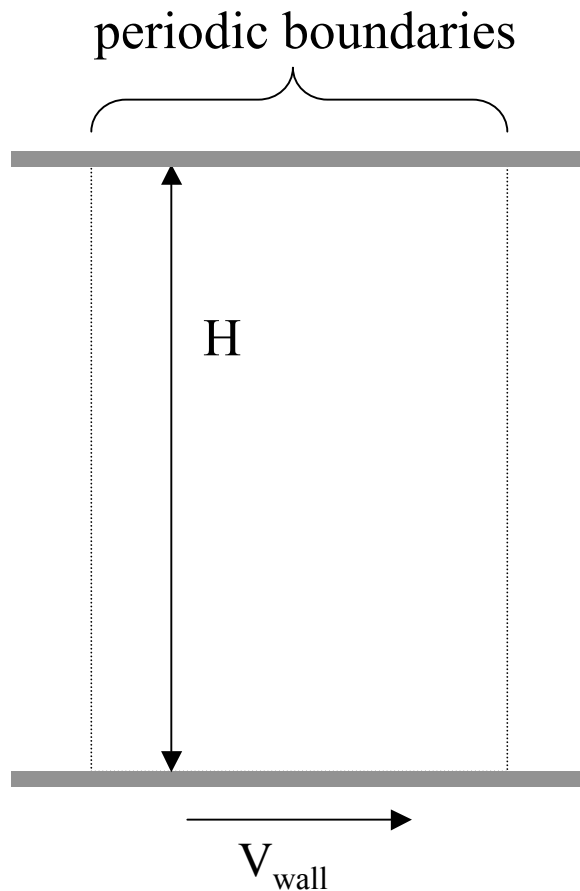
$$\tau_{wall} = -\mu \left( \frac{\partial u}{\partial y} \right)_{y=0} = \mu \left( \frac{V_{wall}}{\sqrt{\pi \nu t}} \right)$$



# Unsteady Flow – Impulsive start-up of a plate

## Problem set-up

## Solver Set-Up



### Material Properties:

$$\rho = 1 \text{ kg/m}^3$$

$$\mu = 0.1 \text{ kg/ms}$$

### Reynolds number:

$$\text{Re} = \rho V_{\text{wall}} L / \mu$$

$$V_{\text{wall}} = 5.605$$

$$L = \mu V_{\text{wall}} / \tau_{\text{wall}}$$

### Boundary Conditions:

Slip wall ( $u = V_{\text{wall}}$ ) on bottom

No-slip wall (top)

Periodicity  $\Delta p = 0$

### Initial Conditions:

$$u = v = p = 0$$

### Exact Solution

$$\tau_{\text{wall}} = 1 \text{ @ } t = 1$$

$$H/L \sim 10$$

### Segregated Solver

### Discretization:

2<sup>nd</sup> order upwind

SIMPLE

### Multigrid

V-Cycle



# Unsteady Flow – Impulsive start-up of a plate

The error CAN be computed with reference to the exact solution  
In this case the computed wall shear stress is plotted

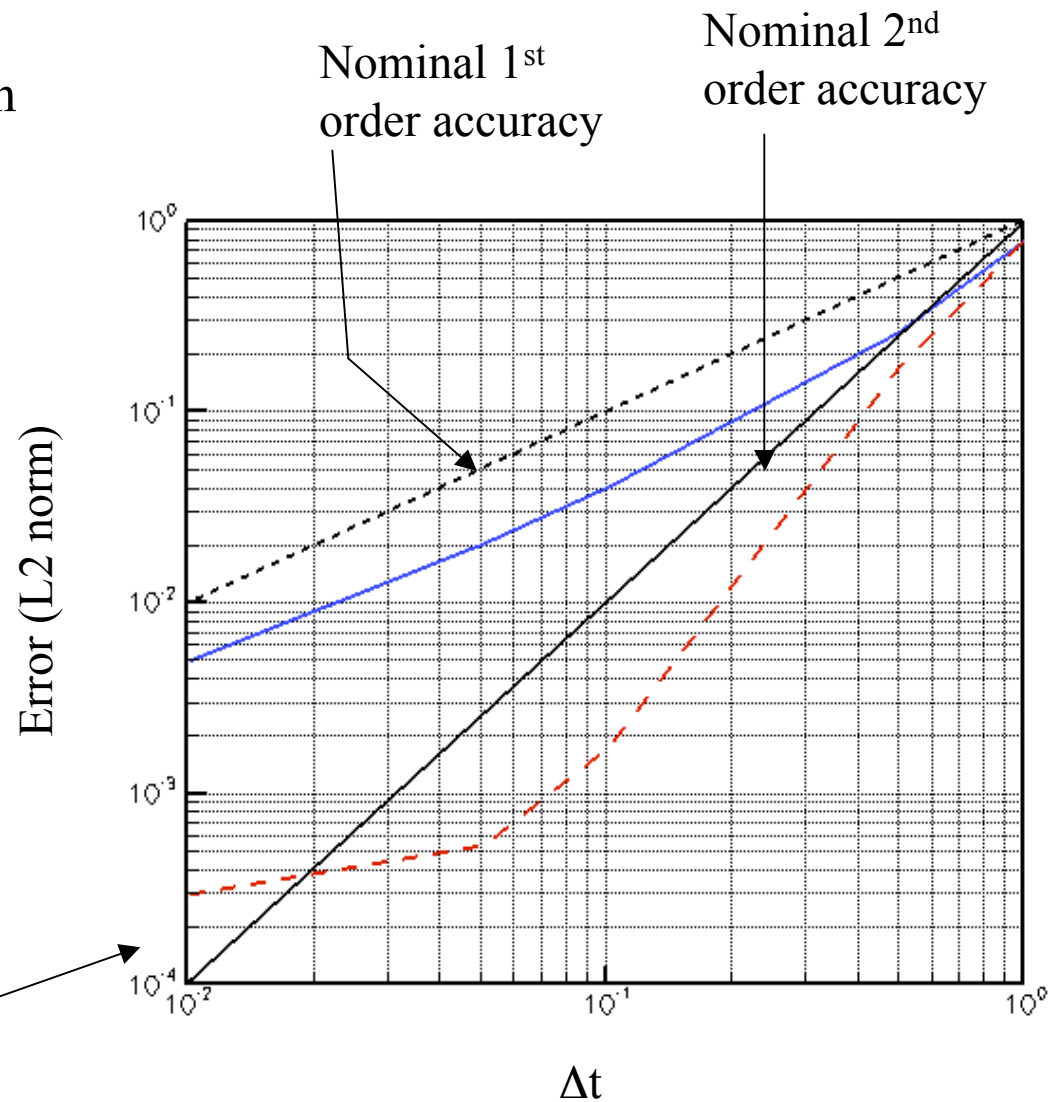
Time discretization

1<sup>st</sup> order

2<sup>nd</sup> order



Influence of the BCs





## Unsteady Flow – Density based formulation

Vector form of the (compressible) NS equations

$$\frac{\partial}{\partial t} \int_V \mathbf{W} dV + \oint [\mathbf{F} - \mathbf{G}] \cdot d\mathbf{A} = \int_V \mathbf{H} dV$$

$$\mathbf{W} = \begin{Bmatrix} \rho \\ \rho u \\ \rho v \\ \rho w \\ \rho E \end{Bmatrix}, \quad \mathbf{F} = \begin{Bmatrix} \rho v \\ \rho v u + p \hat{\mathbf{i}} \\ \rho v v + p \hat{\mathbf{j}} \\ \rho v w + p \hat{\mathbf{k}} \\ \rho v E + p v \end{Bmatrix}, \quad \mathbf{G} = \begin{Bmatrix} 0 \\ \tau_{xi} \\ \tau_{yi} \\ \tau_{zi} \\ \tau_{ij} v_j + \mathbf{q} \end{Bmatrix}$$

Change of variables

$$\frac{\partial \mathbf{W}}{\partial \mathbf{Q}} \frac{\partial}{\partial t} \int_V \mathbf{Q} dV + \oint [\mathbf{F} - \mathbf{G}] \cdot d\mathbf{A} = \int_V \mathbf{H} dV$$

$$\vec{Q} = [p, \vec{V}, T]^T$$

Preconditioning

$$\Gamma \frac{\partial}{\partial t} \int_V \mathbf{Q} dV + \oint [\mathbf{F} - \mathbf{G}] \cdot d\mathbf{A} = \int_V \mathbf{H} dV$$



## Unsteady Flow – Density based formulation

For time-accurate simulations the preconditioning cannot be used (it alters the propagation speed of the acoustic signals)

Time integration:

Implicit - n is the time step loop, k is the inner iteration loop

$\Delta t$  determines the time accuracy,  $\Delta \tau$  is a pseudo-time step determined by stability conditions (a CFL number)

$$\left[ \frac{\Gamma}{\Delta \tau} + \frac{\epsilon_0}{\Delta t} \frac{\partial \mathbf{W}}{\partial \mathbf{Q}} \right] \Delta \mathbf{Q}^{k+1} + \frac{1}{V} \oint [\mathbf{F} - \mathbf{G}] \cdot d\mathbf{A} \\ = \mathbf{H} + \frac{1}{\Delta t} (\epsilon_0 \mathbf{W}^k - \epsilon_1 \mathbf{W}^n + \epsilon_2 \mathbf{W}^{n-1})$$

$$\epsilon_0 = \epsilon_1 = 1/2, \epsilon_2 = 0 \quad \text{First order}$$

$$\epsilon_0 = 3/2, \epsilon_1 = 2, \epsilon_2 = 1/2 \quad \text{Second order}$$



# Reynolds-Averaged Navier-Stokes Equations

$$\frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j} = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} \left( \frac{\mu}{\rho} \frac{\partial u_i}{\partial x_j} \right)$$

Define Reynolds-averaged quantities

$$u_i(x_k, t) = U_i(x_k) + u'(x_k, t)$$

$$U_i(x_k) = \lim_{T \rightarrow \infty} \frac{1}{T} \int_0^T u(x_k, t) dt$$

Substitute and average:

$$\cancel{\frac{\partial U_i}{\partial t}} + U_j \frac{\partial U_i}{\partial x_j} = -\frac{1}{\rho} \frac{\partial P}{\partial x_i} + \frac{\partial}{\partial x_j} \left( \frac{\mu}{\rho} \frac{\partial U_i}{\partial x_j} \right) + \frac{\partial \left( -\overline{u'_i u'_j} \right)}{\partial x_j}$$
$$R_{ij} = -\overline{u'_i u'_j}$$

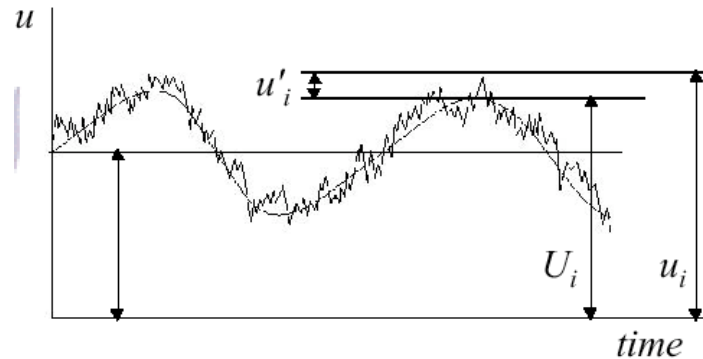
Closure  
problem



# Unsteady RANS?

Every turbulent flow is unsteady BUT not all the unsteadiness is *turbulence*!

RANS averaging based on time average can be applied only to “statistically” steady flows. What if flow has a large scale periodicity (vortex shedding)?



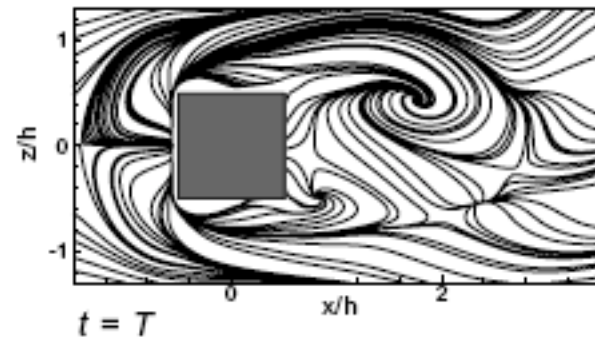
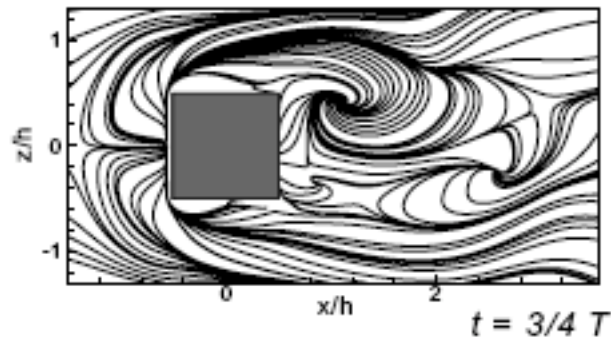
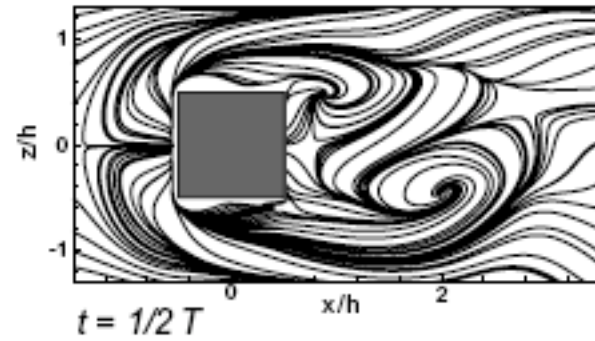
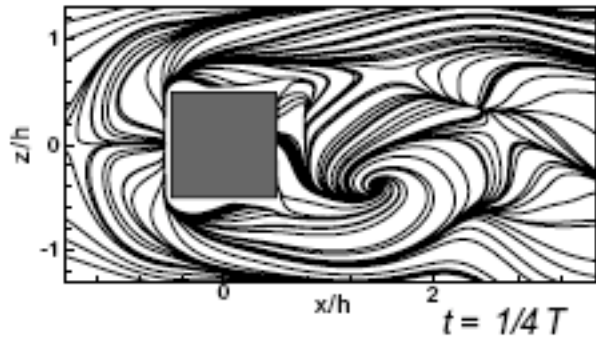
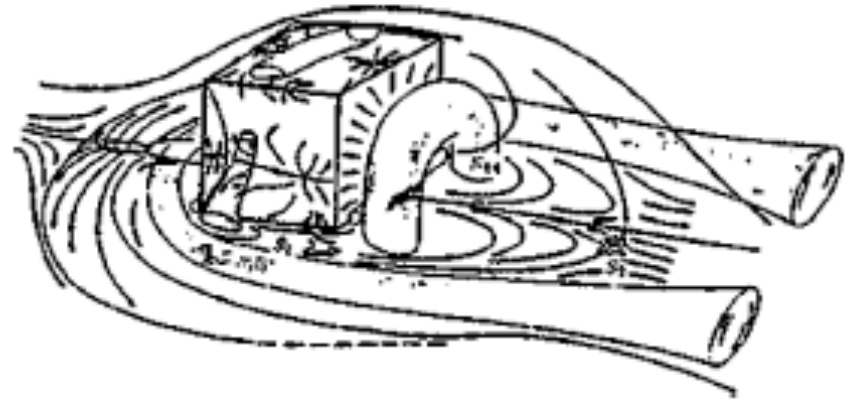
We can define the Reynolds-Averaging procedure in terms of **Ensemble Average**:

$$U_i(x_k, t) = \lim_{N \rightarrow \infty} \frac{1}{N} \sum_{n=1}^N u_i^{(n)}(x_k, t)$$

$$u_i(x_k, t) = U_i(x_k, t) + u'_i(x_k, t)$$



# Turbulent Vortex Shedding



# Turbulent Vortex Shedding

