

**Overhead Slides for**  
**Chapter 16**  
**of**  
**Fundamentals of**  
**Atmospheric Modeling**

**by**

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# Coagulation

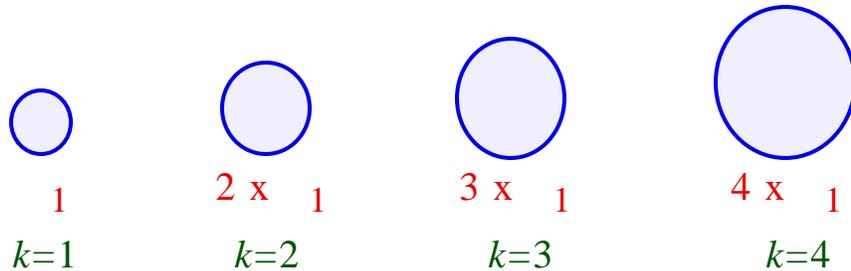
Process by which particles collide and stick together

Integro-differential coagulation equation

$$\frac{dn}{dt} = \frac{1}{2} \int_0^n K(n-n', n') dn' - n \int_0^\infty K(n, n') dn' \quad (16.1)$$

# Coagulation Over Monomer Size Structure

Fig. 16.1. Monomer size structure.



Coagulation equation over monomer size structure

$$\frac{dn_k}{dt} = \frac{1}{2} \sum_{j=1}^{k-1} k-j, j n_{k-j} n_j - n_k \sum_{j=1}^{k,j} k, j n_j \quad (16.2)$$

Rewrite in fully implicit finite difference form

$$\frac{n_{k,t} - n_{k,t-h}}{h} = \frac{1}{2} \sum_{j=1}^{k-1} P_{k,j} - \sum_{j=1}^{k,j} L_{k,j} \quad (16.3)$$

Production rate

$$P_{k,j} = k-j, j n_{k-j} n_j \quad (16.4)$$

Loss rate

$$L_{k,j} = k, j n_k n_j \quad \rightarrow \quad P_{k,j} = L_{k-j,j}$$

Rewrite (16.3) (16.5)

$$n_{k,t} = n_{k,t-h} + \frac{1}{2} h \sum_{j=1}^{k-1} k-j, j n_{k-j,t} n_{j,t} - h \sum_{j=1}^{k,j} k, j n_{k,t} n_{j,t}$$

# Semi-Implicit Coagulation Over Monomer Structure

Write loss rate in semi-implicit form

$$L_{k,j} = k,j n_{k,t} n_{j,t-h} \quad (16.6)$$

Substitute (16.6) into (16.3)

$$n_{k,t} = n_{k,t-h} + \frac{1}{2} h \sum_{j=1}^{k-1} k-j, j n_{k-j,t} n_{j,t-h} - h \sum_{j=1}^{k-1} k,j n_{k,t} n_{j,t-h} \quad (16.7)$$

Rearrange --> number (but not volume) conserving equation

$$n_{k,t} = \frac{n_{k,t-h} + \frac{1}{2} h \sum_{j=1}^{k-1} k-j, j n_{k-j,t} n_{j,t-h}}{1 + h \sum_{j=1}^{k-1} k,j n_{j,t-h}} \quad (16.8)$$

Volume (but not number) conserving equation

$$v_{k,t} = \frac{v_{k,t-h} + h \sum_{j=1}^{k-1} k-j, j v_{k-j,t} n_{j,t-h}}{1 + h \sum_{j=1}^{k-1} k,j n_{j,t-h}} \quad (16.9)$$

where  $v_{k,t} = k n_{k,t}$

# Semi-Implicit Coagulation Over Arbitrary Structure

Volume of intermediate particle

$$V_{i,j} = i + j \quad (16.10)$$

Volume fraction of  $V_{i,j}$  partitioned to each model bin  $k$

$$f_{i,j,k} = \begin{cases} \frac{k+1 - V_{i,j}}{k+1 - k} \frac{k}{V_{i,j}} & k - V_{i,j} < k+1 & k < N_B \\ 1 - f_{i,j,k-1} & k-1 < V_{i,j} < k & k > 1 \\ 1 & V_{i,j} = k & k = N_B \\ 0 & \text{all other cases} & \end{cases}$$

(16.11)

Substitute fractions into (16.9)

$$v_{k,t} = \frac{\sum_{j=1}^k \sum_{i=1}^{k-1} f_{i,j,k} v_{i,t} v_{j,t-h}}{1 + h \sum_{j=1}^k (1 - f_{k,j,k}) v_{j,t-h}} \quad (16.12)$$

# Semi-Implicit Coagulation Over Arbitrary Structure

Substitute  $v = n$  --> Another volume conserving solution

$$n_{k,t} = \frac{n_{k,t-h} + \frac{h}{N_B} \sum_{j=1}^k \sum_{i=1}^{k-1} f_{i,j,k} n_{i,t-h} n_{j,t-h}}{1 + h \sum_{j=1}^k \left(1 - f_{k,j,k}\right) n_{j,t-h}} \quad (16.13)$$

Volume concentration solution when multiple components

$$v_{q,k,t} = \frac{v_{q,k,t-h} + \frac{h}{N_B} \sum_{j=1}^k \sum_{i=1}^{k-1} f_{i,j,k} v_{q,i,t-h} n_{j,t-h}}{1 + h \sum_{j=1}^k \left[ \left(1 - f_{k,j,k}\right) n_{j,t-h} \right]} \quad (16.14)$$

# Coagulation Over Multiple Structures

Internally-mixed structure (I)

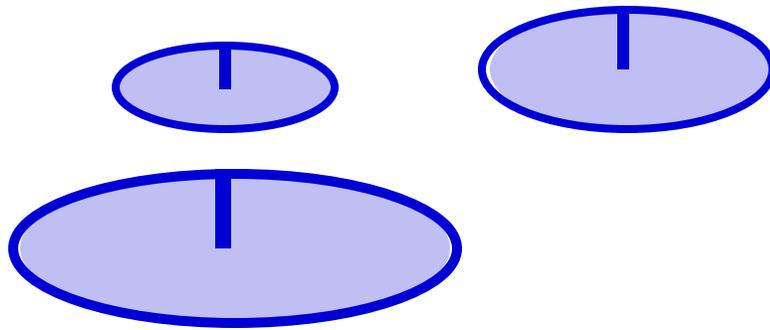
Contains particles with all components

Externally-mixed structure (E)

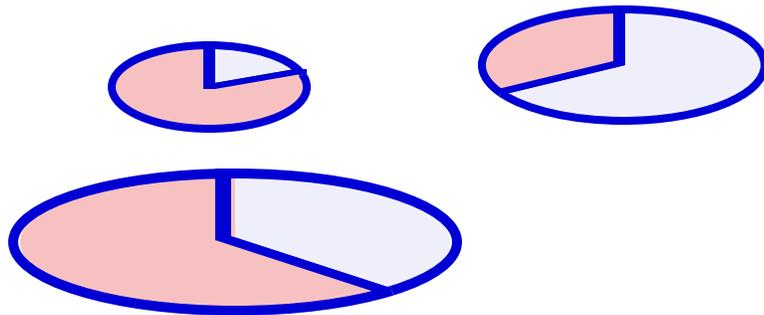
Contains particles with at least one component

Fig. 16.1. Externally- and internally-mixed size structures

E<sub>1</sub>



E<sub>2</sub>



I

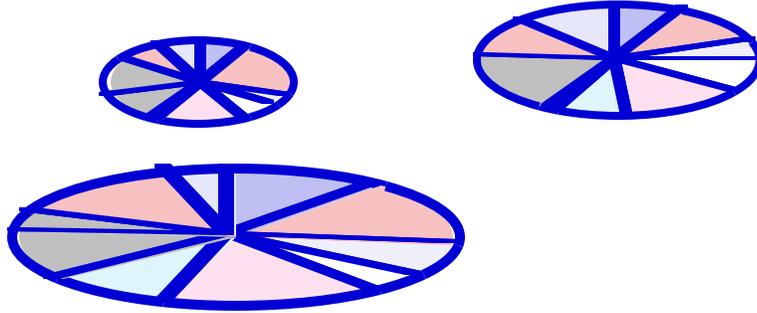


Table 16.1. Changes in number and volume when coagulation occurs among externally- and internally-mixed particles.

Coagulating Pairs	Number			Volume		
	$E_1$	$E_2$	I	$E_1$	$E_2$	I
$E_1$ w/ $E_1$	(-)	---	---	(0)	---	---
$E_1$ w/ $E_2$	(-)	(-)	(+)	(-)	(-)	(+)
$E_1$ w/ I	(-)	---	(0)	(-)	---	(+)
I w/ I	---	---	(-)	---	---	(0)

# Coagulation Over Multiple Structures

Volume concentration of component  $q$  in size bin  $k$  of the  $N^{\text{th}}$  externally-mixed particle

$$v_{q,Nk,t} = \frac{v_{q,Nk,t-h} + \frac{h}{k} \sum_{j=1}^k \sum_{i=1}^{k-1} f_{i,j,k} n_{i,Nj} v_{q,Ni,t} n_{Nj,t-h}}{1 + h \sum_{j=1}^{N_B} \left(1 - f_{k,j,k}\right) n_{k,Nj} n_{Nj,t-h} + \sum_{M=1}^{N_T} \frac{N_{k,Mj} n_{Mj,t-h}}{M N}} \quad (16.15)$$

$N_T$  = number of particle types (external plus internal)

$N, M$  = denote separate particle distributions

$N_B$  = number of size bins

$N_E$  = number of externally-mixed types

$N_V$  = number of volume components

solved for each  $k = 1, N_B, N = 1, N_E$ , and  $q = 1, N_V$ .

Number concentration of externally-mixed particles in bin  $k$

$$n_{Nk,t} = \frac{n_{Nk,t-h} + \frac{h}{k} \sum_{j=1}^k \sum_{i=1}^{k-1} f_{i,j,k} n_{i,Nj} n_{Nj,t-h}}{1 + h \sum_{j=1}^{N_B} \left(1 - f_{k,j,k}\right) n_{k,Nj} n_{Nj,t-h} + \sum_{M=1}^{N_T} \frac{N_{k,Mj} n_{Mj,t-h}}{M N}} \quad (16.16)$$

# Coagulation Over Multiple Structures

Volume concentration of component  $q$  and size  $k$  of the internally-mixed particle, denoted with index number  $N$

$$v_{q,Nk,t} =$$

$$v_{q,Nk,t-h} + h \frac{\sum_{M=1}^{N_T} \sum_{j=1}^k n_{Mj,t-h} \sum_{i=1}^{k-1} f_{i,j,k} N_{i,Mj} v_{q,Ni,t} + \sum_{I=1}^{N_X} \sum_{i=1}^k f_{i,j,k} N_{i,Mj} v_{q,Ii,t}}{1 + h \sum_{M=1}^{N_T} \sum_{j=1}^{N_B} \left(1 - f_{k,j,k}\right) N_{k,Mj} n_{Mj,t-h}}$$

(16.17)

Number concentration in size bin  $k$  of internally-mixed type

$$n_{Nk,t} =$$

$$v_{q,Nk,t-h} + h \frac{\sum_{M=1}^{N_T} \sum_{j=1}^k n_{Mj,t-h} \sum_{i=1}^{k-1} f_{i,j,k} N_{i,Mj} v_{q,Ni,t} + \sum_{I=1}^{N_X} \sum_{i=1}^k f_{i,j,k} N_{i,Mj} v_{q,Ii,t}}{1 + h \sum_{M=1}^{N_T} \sum_{j=1}^{N_B} \left(1 - f_{k,j,k}\right) N_{k,Mj} n_{Mj,t-h}}$$

(16.18)

# Coagulation Kernel

Coagulation kernel (rate coefficient)

Brownian diffusion

Convective Brownian diffusion enhancement

Gravitational collection

Turbulent inertial motion

Turbulent shear

Brownian diffusion

Particles diffuse randomly, collide, and coalesce

Knudsen number

$$\text{Kn}_{a,i} = \frac{a}{r_i} \quad (16.19)$$

Mean free path of an air molecule

$$a = \frac{2a}{a\bar{v}_a} = \frac{2a}{\bar{v}_a} \quad (16.20)$$

Thermal velocity of an air molecule

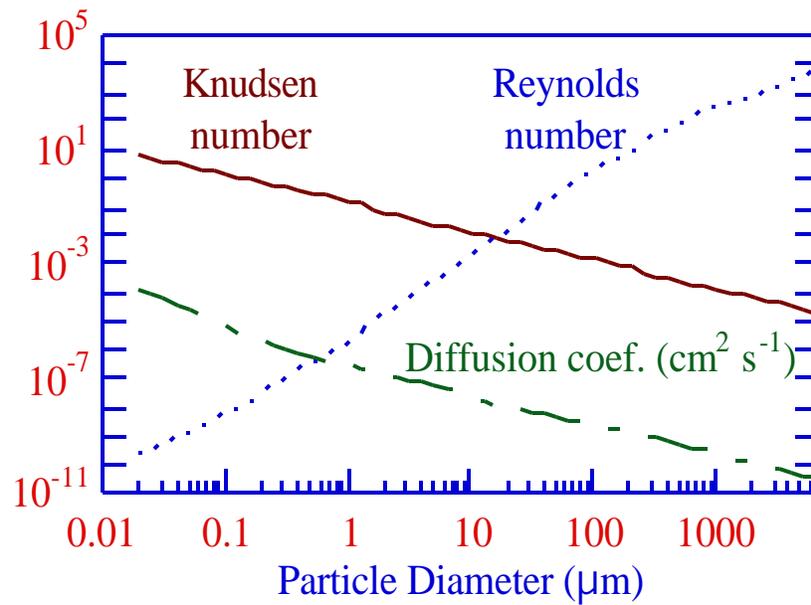
$$\bar{v}_a = \frac{8k_B T}{M}^{1/2} \quad (16.21)$$

Particle Reynolds number

$$\text{Re}_i = 2r_i V_{f,i} / a \quad (16.22)$$

# Particle Properties

Fig. 16.3. Knudsen number for air, Reynolds number, and diffusion coefficient of falling particles as a function of diameter when  $T = 292$  K,  $p_a = 999$  mb, and  $\rho = 1.0$  g cm<sup>-3</sup>.



# Brownian Diffusion Kernel

## Continuum regime

$\text{Kn}_{a,i} \ll 1 \rightarrow r_i \gg a$  and particle resistance to motion is due to viscosity of the air.

## Free molecular regime

$\text{Kn}_{a,i} \gg 10 \rightarrow r_i \ll a$  and particle resistance to motion is due to inertia of air molecules hit by particles.

## Example 16.1.

	$T$	= 288 K
	$p_a$	= 1013 mb
	$r_i$	= 0.1 $\mu\text{m}$ .
---	$\bar{v}_a$	= $4.59 \times 10^4 \text{ cm s}^{-1}$
---	$a$	= $1.79 \times 10^{-4} \text{ g cm}^{-1} \text{ s}^{-1}$
---	$a$	= $0.00123 \text{ g cm}^{-3}$
---	$a$	= $6.34 \times 10^{-6} \text{ cm}$
---	$\text{Kn}_{a,i}$	= 0.63

## Continuum regime Brownian coag. rate ( $\text{cm}^3 \text{ partic. s}^{-1}$ )

$$B_{i,j} = 4 (r_i + r_j) (D_{p,i} + D_{p,j}) \quad (16.23)$$

## Particle diffusion coefficient

$$D_{p,i} = \frac{k_B T}{6 r_i a} G_i \quad (16.24)$$

## Cunningham slip-flow correction to particle resistance to motion

$$G_i = 1 + \text{Kn}_{a,i} \left[ A + B \exp\left(-C / \text{Kn}_{a,i}\right) \right] \quad (16.25)$$

## Brownian Diffusion Kernel

Free molecular regime Brownian coag. rate ( $\text{cm}^3 \text{ partic. s}^{-1}$ )

$$B_{i,j} = (r_i + r_j)^2 \left( \bar{v}_{p,i}^2 + \bar{v}_{p,j}^2 \right)^{1/2} \quad (16.26)$$

Particle thermal velocity

$$\bar{v}_{p,i} = \frac{8k_B T}{\bar{M}_{p,i}}^{1/2} \quad (16.27)$$

Interpolate between continuum and free molecular regimes

$$B_{i,j} = \frac{4 (r_i + r_j) (D_{p,i} + D_{p,j})}{r_i + r_j + \left( \frac{2}{i} + \frac{2}{j} \right)^{1/2} + \frac{4(D_{p,i} + D_{p,j})}{\left( \bar{v}_{p,i}^2 + \bar{v}_{p,j}^2 \right)^{1/2} (r_i + r_j)}} \quad (16.28)$$

Mean distance from center of a sphere reached by particles leaving the sphere's surface and traveling a distance  $p,i$

$$i = \frac{(2r_i + p,i)^3 - (4r_i^2 + \frac{2}{p,i})^{3/2}}{6r_i p,i} - 2r_i \quad (16.29)$$

Particle mean free path (cm)

$$p,i = \frac{2D_{p,i}}{\bar{v}_{p,i}} \quad (16.29)$$

# Brownian Diffusion Enhancement

Eddies created in the wake of a large, falling particle enhance diffusion to the particle surface

Brownian diffusion enhancement coagulation kernel

$$DE_{i,j} = \begin{cases} B_{i,j} 0.45 \text{Re}_j^{1/3} \text{Sc}_{p,i}^{1/3} & \text{Re}_j \leq 1; r_j \leq r_i \\ B_{i,j} 0.45 \text{Re}_j^{1/2} \text{Sc}_{p,i}^{1/3} & \text{Re}_j > 1; r_j \leq r_i \end{cases} \quad (16.30)$$

Particle Schmidt number

$$\text{Sc}_{p,i} = a/D_{p,i} \quad (16.31)$$

## Differential Fall Velocities

Collision and coalescence when one particle falls faster than and catches up with another

Differential fall velocity coagulation kernel

$K_{i,j}^{GC} = E_{i,j} (r_i + r_j)^2  V_{f,i} - V_{f,j}  \quad (16.32)$
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Collection (coalescence) efficiency

$$E_{i,j} = \frac{60 E_{V,i,j} + E_{A,i,j} \text{Re}_j}{60 + \text{Re}_j} \quad r_j \geq r_i \quad (16.33)$$

$E_{i,j}$  simplifies to

$E_{V,i,j}$  when  $\text{Re}_j \ll 1$  (viscous flows)

$E_{A,i,j}$  when  $\text{Re}_j \gg 1$  (potential flows)

$$E_{V,i,j} = \begin{cases} 1 + \frac{0.75 \ln(2K_{i,j})}{K_{i,j} - 1.214} & K_{i,j} > 1.214 \\ 0 & K_{i,j} \leq 1.214 \end{cases} \quad (16.34)$$

$$E_{A,i,j} = \frac{K_{i,j}^2}{(K_{i,j} + 0.5)^2}$$

Stokes number

$$K_{i,j} = V_{f,i} |V_{f,j} - V_{f,i}| / r_j g \quad r_j \geq r_i$$

# Turbulent Inertia and Shear

Coagulation kernel due to turbulent inertial motion

Collision between drops moving relative to air

$$\frac{TI}{i,j} = \frac{k}{g} \frac{3/4}{1/4} (r_i + r_j)^2 |V_{f,i} - V_{f,j}| \quad (16.35)$$

Coagulation kernel due to turbulent shear

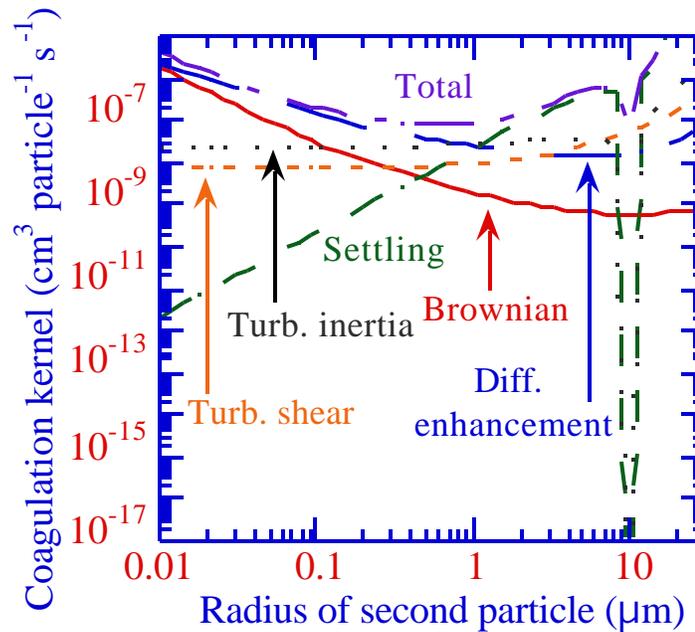
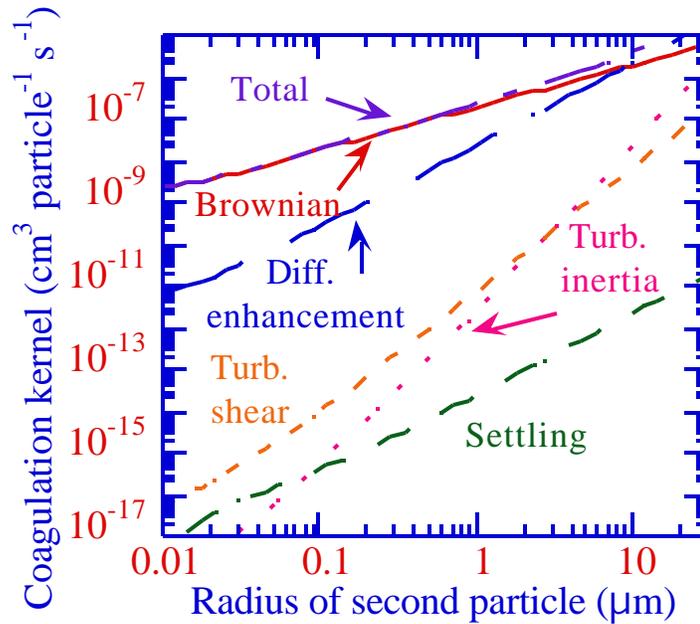
Collisions due to spatial variations in turbulent velocities of drops moving with air

$$\frac{TS}{i,j} = \frac{8}{15} \frac{k}{a}^{1/2} (r_i + r_j)^3 \quad (16.36)$$

$k$  = dissipation rate of turbulent energy per gram of medium ( $\text{cm}^2 \text{s}^{-3}$ )

# Comparisons of Coagulation Kernels

Figs. 16.4 a and b. Coagulation kernels when particle of (a) 0.01  $\mu\text{m}$  and (b) 10  $\mu\text{m}$  in radius coagulate at 298 K.



# Smoluchowski's (1918) Solution

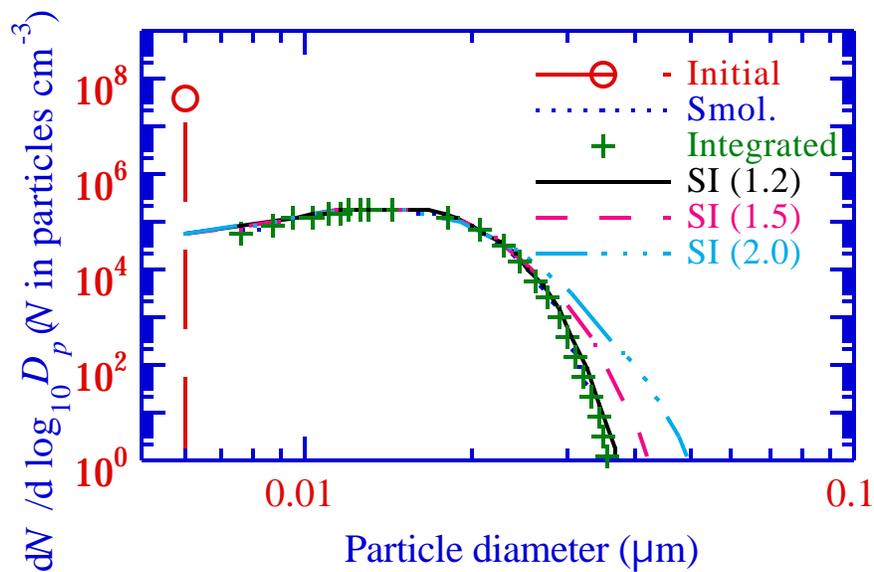
Assume monomer size distribution, constant rate, and  
initial monodisperse distribution

$$n_{k,t} = \frac{n_{T,t-h} (0.5h n_{T,t-h})^{k-1}}{(1 + 0.5h n_{T,t-h})^{k+1}} \quad (16.37)$$

Coagulation kernel

$$= \frac{8k_B T}{3a} \quad (16.38)$$

Fig. 16.5. Comparison of Smoluchowski's solution, an integrated solution, and three semi-implicit solutions.



# Self-Preserving Solution

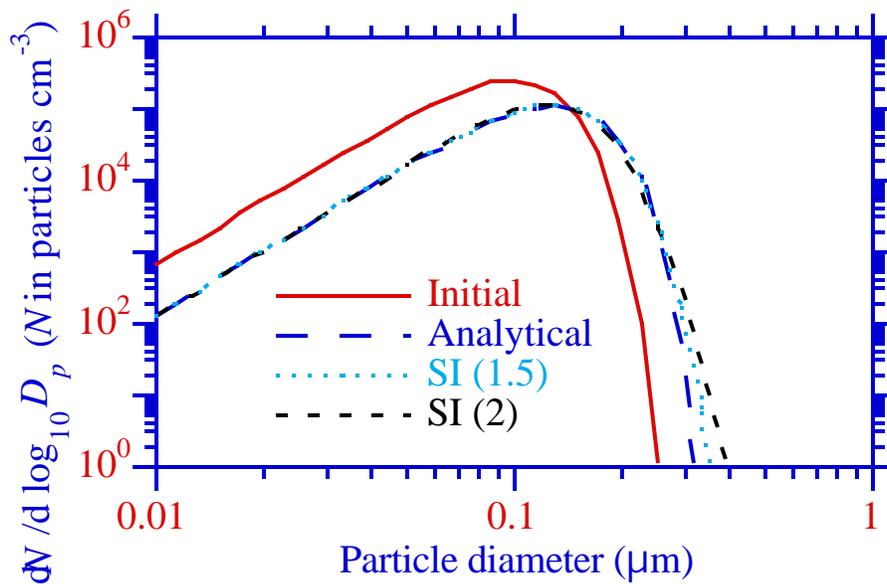
Self-preserving size distribution

$$n_{i,t-h} = \frac{n_{T,t-h}}{p} \exp \left( -\frac{i}{p} \right) \quad (16.39)$$

Solution to coagulation over self-preserving distribution

$$n_{i,t} = \frac{n_{T,t-h}}{\left(1 + 0.5h \frac{i}{p} n_{T,t-h}\right)^2} \exp \left( -\frac{i/p}{1 + 0.5h \frac{i}{p} n_{T,t-h}} \right) \quad (16.40)$$

Fig. 16.6. Self-preserving versus semi-implicit solutions



# Effect of Coagulation

Coagulation affects the number concentration of particles smaller than  $0.2 \mu\text{m}$  in size

Fig. 16.7. Estimated change in size-distributed aerosol number and volume at Claremont over a 24-hour period when coagulation, alone, was considered.

